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<b>(51) International Patent Classification <sup>5</sup> :</b> <b>C08L 69/00, 67/02, 53/00</b> <b>C08L 51/00, 71/12, 101/00</b>	<b>A2</b>	<b>(11) International Publication Number:</b> <b>WO 93/19128</b> <b>(43) International Publication Date:</b> 30 September 1993 (30.09.93)												
<b>(21) International Application Number:</b> PCT/US93/02176 <b>(22) International Filing Date:</b> 10 March 1993 (10.03.93)  <b>(30) Priority data:</b> <table border="0"><tr><td>07/850,324</td><td>10 March 1992 (10.03.92)</td><td>US</td></tr><tr><td>07/850,329</td><td>10 March 1992 (10.03.92)</td><td>US</td></tr><tr><td>07/850,335</td><td>10 March 1992 (10.03.92)</td><td>US</td></tr><tr><td>07/851,371</td><td>10 March 1992 (10.03.92)</td><td>US</td></tr></table> <b>(71) Applicant:</b> THE DOW CHEMICAL COMPANY [US/US]; 2030 Dow Center, Abbott Road, Midland, MI 48640 (US). <b>(72) Inventor:</b> LAUGHNER, Michael, K. ; 1403 North Road, Lake Jackson, TX 77566 (US). <b>(74) Agent:</b> LANGWORTHY, John, A.; The Dow Chemical Company, Patent Dept., B-1211, Freeport, TX 77541 (US).		07/850,324	10 March 1992 (10.03.92)	US	07/850,329	10 March 1992 (10.03.92)	US	07/850,335	10 March 1992 (10.03.92)	US	07/851,371	10 March 1992 (10.03.92)	US	<b>(81) Designated States:</b> CA, JP, European patent (AT, BE, CH, DE, DK, ES, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE).  <b>Published</b> <i>Without international search report and to be republished upon receipt of that report.</i>  <div style="text-align: center;"><b>RECEIVED</b> <b>JUL 6 - 2005</b> <b>IPO</b> <b>GENERAL ELECTRIC CO.</b></div>
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<b>(54) Title:</b> POLYMERS AND POLYMER BLENDS MODIFIED WITH POLY(PHENYLENE ETHER)  <b>(57) Abstract</b> <p>A matrix resin such as a polycarbonate/polyester blend, a polycarbonate, a vinyl aromatic copolymer or an acrylate polymer or copolymer is admixed in a composition with poly(phenylene ether), and/or with a poly(phenylene ether) concentrate containing poly(phenylene ether), polystyrene, a vinyl aromatic copolymer, polyamide, polycarbonate, polyester, poly(alkyl acrylate), and/or poly(alkyl methacrylate). The compositions may also optionally contain additional vinyl aromatic copolymer as a separate component, impact modifiers, thermoplastic molding materials including polystyrene, polyolefin, polyamide, poly(vinyl chloride), polyurethane, poly(methyl methacrylate) and polyacetal, and conventional additives such as dyes and pigments. The compositions when molded, particularly when the poly(phenylene ether) content thereof is low (for example, 5 weight percent or less) show a desirably low gloss, and a desirable balance of other properties.</p>														

## POLYMERS AND POLYMER BLENDS MODIFIED WITH POLY(PHENYLENE ETHER)

This invention relates to compositions of thermoplastic polymers and polymer blends which have been modified with poly(phenylene ether), and to methods of melt processing and molding such compositions.

It is frequently desired that articles molded from thermoplastic polymers and polymer blends have low gloss. It is known that gloss can be reduced in a molded article by, for example, adding a filler such as talc to the molding composition, lowering the temperature of the mold, or etching on the mold a pattern which becomes imprinted on the surface of the article. It has been found, however, that an article characterized by reduced gloss can also be obtained by molding it from the poly(phenylene ether) modified compositions of this invention.

In one aspect, this invention involves a composition of matter containing, in admixture,

- (a/a) a blend of polycarbonate and polyester; and  
(b/a) (i) poly(phenylene ether), (ii) a blend of poly(phenylene ether) with one or more of components (A) to (G), as follows: (A) polystyrene, (B) a random, alternate, block, hydrogenated block or grafted copolymer prepared from a vinyl aromatic compound and one or more members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl methacrylate, ethylene/propylene/diene copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an oxazoline compound, (C) polyamide, (D) polycarbonate, (E) polyester, (F) poly(alkyl acrylate), and (G) poly(alkyl methacrylate), or (iii) a mixture thereof.

In another aspect, this invention involves a method of molding an article comprising (I) forming a composition by melting in a molding machine components (a/a) and (b/a) which have not previously been melted together, said components (a/a) and (b/a) comprising

- (a/a) a blend of polycarbonate and polyester; and  
(b/a) (i) poly(phenylene ether), (ii) a blend of poly(phenylene ether) with one or more of components (A) to (G), as follows: (A) polystyrene, (B) a random, alternate, block, hydrogenated block or grafted copolymer prepared from a vinyl aromatic compound and one or more members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl methacrylate, ethylene/propylene/diene copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an oxazoline compound, (C) polyamide, (D) polycarbonate, (E) polyester, (F) poly(alkyl acrylate), and (G) poly(alkyl methacrylate), or (iii) a mixture thereof; and

(II) molding said article from said composition.

In a further aspect, this invention involves a composition of matter containing, in admixture,

(a/b) polycarbonate; and

5 (b/b) a blend of poly(phenylene ether) with one or more of components (1) to (7), as follows: (1) polystyrene, (2) a random, alternate, block, hydrogenated block or grafted copolymer prepared from a vinyl aromatic compound and one or more members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl methacrylate, ethylene/propylene/diene  
10 copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an oxazoline compound, (3) polyamide, (4) polycarbonate, (5) polyester, (6) poly(alkyl acrylate), and (7) poly(alkyl methacrylate).

In a further aspect, this invention involves a method of molding an article comprising (I) forming a composition by melting in a molding machine components (a/b) and  
15 (b/b) which have not previously been melted together, said components (a/b) and (b/b) comprising

(a/b) polycarbonate; and

(b/b) a blend of poly(phenylene ether) with one or more of components (1) to (7), as follows: (1) polystyrene, (2) a random, alternate, block, hydrogenated block or grafted copolymer prepared from a vinyl aromatic compound and one or more  
20 members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl methacrylate, ethylene/propylene/diene copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an oxazoline compound, (3) polyamide, (4) polycarbonate, (5) polyester, (6)  
25 poly(alkyl acrylate), and (7) poly(alkyl methacrylate); and

(II) molding said article from said composition.

In a further aspect, this invention involves a composition of matter containing, in admixture,

(a/c) a random, alternate, block or grafted copolymer prepared from a vinyl aromatic  
30 compound and one or more members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl methacrylate, ethylene/propylene/diene copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an oxazoline compound; and

(b/c) (i) poly(phenylene ether); (ii) a blend of poly(phenylene ether) with one or more  
35 of components (A) to (G), as follows: (A) polystyrene, (B) a random, alternate, block, hydrogenated block or grafted copolymer prepared from a vinyl aromatic compound and one or more members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl

methacrylate, ethylene/propylene/diene copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an oxazoline compound, (C) polyamide, (D) polycarbonate, (E) polyester, (F) poly(alkyl acrylate), and (G) poly(alkyl methacrylate); or (iii) a mixture thereof.

In a further aspect, this invention involves a method of molding an article comprising (I) forming a composition by melting in a molding machine components (a/c) and (b/c) which have not previously been melted together, said components (a/c) and (b/c) comprising

- (a/c) a random, alternate, block or grafted copolymer prepared from a vinyl aromatic compound and one or more members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl methacrylate, ethylene/propylene/diene copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an oxazoline compound; and
- (b/c) a blend of poly(phenylene ether) with one or more of components (1) to (7), as follows: (1) polystyrene, (2) a random, alternate, block, hydrogenated block or grafted copolymer prepared from a vinyl aromatic compound and one or more members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl methacrylate, ethylene/propylene/diene copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an oxazoline compound, (3) polyamide, (4) polycarbonate, (5) polyester, (6) poly(alkyl acrylate), and (7) poly(alkyl methacrylate); and

(II) molding said article from said composition.

In a further aspect, this invention involves a composition of matter containing, in admixture,

- (a/d) (i) poly(alkyl acrylate), (ii) poly(alkyl methacrylate), (iii) a copolymer prepared from (A) an alkyl acrylate, an alkyl methacrylate, or a mixture thereof, and (B) one or more ethylenically unsaturated monomers, or (iv) a mixture thereof; and
- (b/d) (i) poly(phenylene ether), (ii) a blend of poly(phenylene ether) with one or more of components (A) to (G), as follows: (A) polystyrene, (B) a random, alternate, block, hydrogenated block or grafted copolymer prepared from a vinyl aromatic compound and one or more members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl methacrylate, ethylene/propylene/diene copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an oxazoline compound, (C) polyamide, (D) polycarbonate, (E) polyester, (F) poly(alkyl acrylate), and (G) poly(alkyl methacrylate), or (iii) a mixture thereof.

In a further aspect, this invention involves a method of molding an article comprising (I) forming a composition by melting in a molding machine components (a/d) and

(b/d) which have not previously been melted together, said components (a/d) and (b/d) comprising

(a/d) (i) poly(alkyl acrylate), (ii) poly(alkyl methacrylate), (iii) a copolymer prepared from (A) an alkyl acrylate, an alkyl methacrylate, or a mixture thereof, and (B) one or more ethylenically unsaturated monomers, or (iv) a mixture thereof; and

(b/d) (i) poly(phenylene ether), (ii) a blend of poly(phenylene ether) with one or more of components (A) to (G), as follows: (A) polystyrene, (B) a random, alternate, block, hydrogenated block or grafted copolymer prepared from a vinyl aromatic compound and one or more members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl methacrylate, ethylene/propylene/diene copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an oxazoline compound, (C) polyamide, (D) polycarbonate, (E) polyester, (F) poly(alkyl acrylate), and (G) poly(alkyl methacrylate), or (iii) a mixture thereof; and

(II) molding said article from said composition.

It has been found that not only does an article molded from a composition of this invention exhibit a desirably low level of gloss, but such an article also exhibits lower gloss than does an article molded at the same molding conditions from a composition not containing the same components as the poly(phenylene ether)-modified compositions of this invention. In general, molding an article at a higher temperature increases the gloss of such article as compared with the result of lower temperature molding conditions. The low gloss property of the compositions of this invention therefore makes it possible to mold an article at high temperature, as required for example by a complicated mold, while still obtaining a part which is characterized by low gloss. This makes it possible, for example, to more easily produce low gloss, thin-walled parts.

The compositions of this invention are useful, for example, in the production of films, fibers, extruded sheets, multi-layer laminates and molded or shaped articles of virtually all varieties, especially appliance and instrument housings, motor vehicle body panels and other parts and components for use in the automotive and electronics industries, such as radios and pagers. The methods of this invention are useful for preparing compositions and molded articles having applications which are the same as or similar to the foregoing.

The compositions of this invention include those in which (a/a) a blend of polycarbonate and polyester, has been admixed in a composition with (b/a) (i) poly(phenylene ether) and/or (ii) a poly(phenylene ether) blend. The compositions of this invention may optionally contain one or more of the following: (c/a) a vinyl aromatic copolymer, (d/a) an elastomeric impact modifier, and (e/a) a thermoplastic molding polymer selected from polystyrene, polyolefin, polyamide, poly(vinyl chloride), polyurethane, poly(methyl methacrylate) and polyacetal. Suitable ranges of content for components (a/a) to (e/a) in the

compositions of this invention, expressed in parts by weight of the total composition, are as follows:

- 5 (a/a) polycarbonate/polyester blend from about 10 parts to about 98 parts, advantageously from about 20 parts to about 97 parts, preferably from about 35 parts to about 96 parts, more preferably from about 50 parts to about 95 parts, and most preferably from about 65 parts to about 95 parts,
- 10 (b/a) (i) poly(phenylene ether) from about 0.2 part to about 30 parts, advantageously from about 0.2 part to about 20 parts, preferably from about 0.2 part to about 15 parts, more preferably from about 0.2 part to about 10 parts, and most preferably from about 0.2 part to about 5 parts,
- 15 (b/a) (ii) poly(phenylene ether) blend from about 0.5 part to about 60 parts, advantageously from about 1 part to about 40 parts, preferably from about 1 part to about 30 parts, more preferably from about 1 part to about 25 parts, and most preferably from about 1 part to about 20 parts, provided the resulting poly(phenylene ether) content in the final composition is as set forth in (b)(i), above,
- 20 (c/a) vinyl aromatic copolymer up to about 95 parts, and preferably from about 1 to about 70 parts,
- (d/a) elastomeric impact modifier up to about 30 parts, and preferably from about 1 to about 15 parts, and
- (e/a) thermoplastic molding polymer up to about 95 parts, and preferably from about 1 to about 70 parts.

25 The polycarbonate/polyester blend may be about 1 parts to about 99 parts, advantageously from about 25 parts to about 97 parts, preferably from about 35 parts to about 95 parts, more preferably from about 50 parts to about 95 parts, and most preferably from about 60 parts to about 90 parts polycarbonate, with the balance being polyester.

30 The compositions of this invention also include those in which (a/b) polycarbonate has been admixed in a composition with (b/b) a poly(phenylene ether) blend. The compositions of this invention may optionally contain one or more of the following: (c/b) a vinyl aromatic copolymer, (d/b) an elastomeric impact modifier, and (e/b) a thermoplastic molding polymer selected from polystyrene, polyolefin, polyamide, poly(vinyl chloride), polyurethane and polyacetal. Suitable ranges of content for components (a/b) to (e/b) in the compositions of this  
35 invention, expressed in parts by weight of the total composition, are as follows:

- (a/b) polycarbonate from about 10 parts to about 98 parts, advantageously from about 15 parts to about 95 parts, preferably from about 25 parts to about

93 parts, more preferably from about 35 parts to about 90 parts, and most preferably from about 45 parts to about 90 parts,

- (b/b) poly(phenylene ether) blend from about 0.5 part to about 60 parts, advantageously from about 1 part to about 40 parts, preferably from about 1 part to about 30 parts, more preferably from about 1 part to about 25 parts, and most preferably from about 1 part to about 20 parts, provided the resulting poly(phenylene ether) content in the final composition is from about 0.2 part to about 30 parts, advantageously from about 0.2 part to about 20 parts, preferably from about 0.2 part to about 15 parts, more preferably from about 0.2 part to about 10 parts, and most preferably from about 0.2 part to about 5 parts,
- (c/b) vinyl aromatic copolymer up to about 95 parts, and preferably from about 1 to about 70 parts,
- (d/b) elastomeric impact modifier up to about 30 parts, and preferably from about 1 to about 15 parts, and
- (e/b) thermoplastic molding polymer up to about 95 parts, and preferably from about 1 to about 70 parts.

The compositions of this invention also include those in which (a/c) a vinyl aromatic copolymer has been admixed in a composition with (b/c) (i) poly(phenylene ether) and/or (ii) a poly(phenylene ether) blend. The compositions of this invention may optionally contain one or more of the following: (c/c) an elastomeric impact modifier, and (d/c) a thermoplastic molding polymer selected from polyester, polystyrene, polyolefin, polyamide, poly(vinyl chloride), polyurethane and polyacetal. Suitable ranges of content for components (a/c) to (d/c) in the compositions of this invention, expressed in parts by weight of the total composition, are as follows:

- (a/c) vinyl aromatic copolymer from about 10 parts to about 98 parts, advantageously from about 15 parts to about 98 parts, preferably from about 25 parts to about 95 parts, more preferably from about 30 parts to about 93 parts, and most preferably from about 35 parts to about 93 parts,
- (b/c) (i) poly(phenylene ether) from about 0.2 part to about 30 parts, advantageously from about 0.5 part to about 20 parts, preferably from about 1 part to about 10 parts, more preferably from about 1 part to about 8 parts, and most preferably from about 1 part to about 5 parts,
- (b/c) (ii) poly(phenylene ether) blend from about 0.5 part to about 60 parts, advantageously from about 1 part to about 40 parts, preferably from about 1 part to about 30 parts, more preferably from about 1 part to about 25 parts, and most preferably from about 1 part to about 20

parts, provided the resulting poly(phenylene ether) content in the final composition is as set forth in (b)(i), above,

(c/c) elastomeric impact modifier up to about 30 parts, and preferably from about 1 to about 15 parts, and

5 (d/c) thermoplastic molding polymer up to about 95 parts, and preferably from about 1 to about 70 parts.

The compositions of this invention also include those in which (a/d) an acrylate polymer has been admixed in a composition with (b/d) (i) poly(phenylene ether) and/or (ii) a poly(phenylene ether) blend. The compositions of this invention may optionally contain one or  
10 more of the following: (c/d) a vinyl aromatic copolymer, (d/d) an elastomeric impact modifier, and (e/d) a thermoplastic molding polymer selected from polycarbonate, polyester, polystyrene, polyolefin, polyamide, poly(vinyl chloride), polyurethane and polyacetal. Suitable ranges of content for components (a/d) to (e/d) in the compositions of this invention, expressed in parts by weight of the total composition, are as follows:

15 (a/d) acrylate polymer from about 5 parts to about 99.8 parts, advantageously from about 10 parts to about 96 parts, preferably from about 15 parts to about 95 parts, more preferably from about 20 parts to about 93 parts, and most preferably from about 25 parts to about 90 parts,

20 (b/d) (i) poly(phenylene ether) from about 0.2 part to about 30 parts, advantageously from about 0.5 part to about 25 parts, preferably from about 1 part to about 15 parts, more preferably from about 1 part to about 10 parts, and most preferably from about 1 part to about 5 parts,

(b/d) (ii) poly(phenylene ether) blend from about 0.5 part to about 60 parts,  
25 advantageously from about 1 part to about 40 parts, preferably from about 1 part to about 30 parts, more preferably from about 1 part to about 25 parts, and most preferably from about 1 part to about 20 parts, provided the resulting poly(phenylene ether) content in the final composition is as set forth in (b)(i), above,

30 (c/d) vinyl aromatic copolymer up to about 95 parts, and preferably from about 1 to about 70 parts,

(d/d) elastomeric impact modifier up to about 30 parts, and preferably from about 1 to about 15 parts, and

(e/d) thermoplastic molding polymer up to about 95 parts, and  
35 preferably from about 1 to about 70 parts.

Also included within this invention are the reaction products, if any, of the above named components when admixed in the compositions of this invention. The number of parts



by weight of the various components which make up the compositions of this invention may, but need not, total to 100.

Preparation of the compositions of this invention can be accomplished by any suitable mixing means known in the art. Typically the substances to be admixed with the polycarbonate/polyester blend are dry blended in particulate form with sufficient agitation to  
5 obtain thorough distribution thereof. If desired, the dry-blended formulation can further be melt mixed, for example in an extruder with or without a vacuum, or otherwise compounded with additional substances. Apparatus which can be used in the blending process include, for example, mixing rolls, a dough-mixer or a Banbury mixer.

10 When softened or melted by the application of heat, the compositions of this invention can undergo fabrication and can therein be formed or molded using conventional techniques such as compression, injection molding, gas assisted injection molding, calendering, vacuum forming, thermoforming, extrusion and/or blow molding techniques, alone or in combination. The compositions can also be formed, spun or drawn into films, fibers, multi-  
15 layer laminates or extruded sheets, or can be compounded with one or more organic or inorganic substances, on any machine suitable for such purpose.

Articles molded from compositions prepared within the ranges of content stated above exhibit a desirably low level of gloss.

A polycarbonate, such as an aromatic polycarbonate, can be prepared from an  
20 aromatic dihydroxy compound such as a bisphenol, and a carbonate precursor such as a disubstituted carbonic acid derivative, a haloformate (such as a bishaloformate of a glycol or dihydroxy benzene) or a carbonate ester. These components are often reacted by means of the phase boundary process in which the dihydroxy compound is dissolved and deprotonated in an aqueous alkaline solution and the carbonate precursor is dissolved in an organic solvent. The  
25 aqueous alkaline solution has a pH of 7.01 or more and can be formed in water from a caustic soda, such as NaOH, or from other bases such as those included in the alkali metal and alkaline earth metal phosphates, bicarbonates, oxides and hydroxides. These components are often reacted by means of a mixture prepared initially from the aromatic dihydroxy compound, water and a non-reactive organic solvent immiscible with water selected from among those in  
30 which the carbonate precursor and polycarbonate product are soluble. Representative solvents include chlorinated hydrocarbons such as methylene chloride, 1,2-dichloroethane, tetrachloroethane, chlorobenzene, and chloroform, to which tetrahydrofuran, dioxane, nitrobenzene, dimethyl sulfoxide, xylene, cresol or anisole may be added, if desired. Caustic soda or other base is then added to the reaction mixture to adjust the pH of the mixture to a  
35 level at which the dihydroxy compound is activated to dianionic form. A reducing agent such as sodium sulfite or sodium dithionite can also be advantageously added to the reaction mixture as well.

A carbonate precursor is contacted with an agitated mixture of the aqueous alkaline solution of the dihydroxy compound, and, for such purpose, the carbonate precursor can be bubbled into the reaction mixture in the form of a gas, or can be dissolved and introduced in solution form. The mixture is agitated in a manner which is sufficient to disperse or suspend droplets of the solvent containing the carbonate precursor in the aqueous alkaline solution. Reaction at the interface of the organic and aqueous phases created by such agitation yields the bis(carbonate precursor) ester of the dihydroxy compound. For example, if the carbonate precursor is a carbonyl halide such as phosgene, the products of this initial phase of the process are monomers or oligomers which are either mono- or dichloroformates, or contain a phenolate ion at each terminus. These intermediate mono- and oligocarbonates dissolve in the organic solvent as they form, and they can then be condensed to a higher molecular weight polycarbonate by contact with a coupling catalyst of which the following are representative: a tertiary amine such as triethyl amine or dimethyl amino pyridine; a hindered secondary amine such as diisopropyl amine; a cyclic aza compound such as 2,2,6,6-tetramethyl piperidine or 1,2-dimethylimidazole; an amidine or aminoamidine compound such as 1-methyl-2-phenyliminopyrrolidine; an isourea compound such as N,N-dibutyl-N'-phenyl-o-methylisourea; an iminoether or iminocarboxylate compound such as 1-aza-2-methoxy-1-cycloheptene or t-butyl-cyclohexyliminoacetate; or a phosphonium, sulfonium, arsonium or quaternary ammonium compound. Such a catalyst may be added to the reaction mixture before or after it is contacted with a carbonate precursor.

The reaction can be run at a pH of 7.01 to 14, and at a temperature between 0°C-100°C, although usually not in excess of the boiling point (reflux temperature) of the solvent used. Frequently, the reaction is run at a temperature of about 0°C to about 45°C.

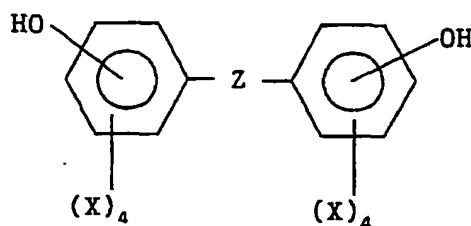
Upon completion of polymerization, the organic and aqueous phases are separated to allow purification of the organic phase and recovery of the polycarbonate product therefrom. The organic phase is washed as needed in a centrifuge with dilute base, water and/or dilute acid until free of unreacted monomer, residual process chemicals and/or other electrolytes. Recovery of the polycarbonate product can be effected by spray drying, steam devolatilization, direct devolatilization in a vented extruder, or precipitation by use of an anti-solvent such as toluene, cyclohexane, heptane, methanol, hexanol, or methyl ethyl ketone.

In the melt process for preparation of polycarbonate, aromatic diesters of carbonic acid are condensed with an aromatic dihydroxy compound in a transesterification reaction in the presence of a basic catalyst such as sodium methylate, sodium bisphenolate, calcium acetate, phenyl benzoate, N-stearoylphenothiazine, quaternary ammonium chloride, an alkaline(hydroxy)fluoroborate, an alkali metal salt of benzoic acid, an iminocarboxylic acid, or basic metal oxides such as zinc, lead or antimony oxide. The reaction is typically run at 250°C-300°C under vacuum at a progressively reduced pressure of 1-100 mm Hg. The reaction is run in the absence of solvent and typically yields lower viscosity grades of polycarbonate.

Aromatic polycarbonate can also be prepared in a homogeneous solution through a process in which a carbonate precursor, such as phosgene, is contacted with a solution containing an aromatic dihydroxy compound, a chlorinated hydrocarbon solvent and a substance, such as pyridine, dimethyl aniline or CaOH, which acts as both acid acceptor and  
 5 condensation catalyst. Washing with acidified water removes the pyridine and its hydrochloride, and precipitation and repulping with an antisolvent such as heptane followed by filtration and distillation removes oligomers and unreacted monomer.

Yet another process for the preparation of aromatic polycarbonate is the polymerization of cyclic oligomers having a weight average molecular weight of approximately  
 10 1,300 at 200°C-300°C, using a catalyst such as lithium stearate or tetramethylammonium tetraphenylborate.

Examples of some dihydroxy compounds suitable for the preparation of aromatic polycarbonate include variously bridged, substituted or unsubstituted aromatic diols (or mixtures thereof) represented by the formula



wherein:

- (I) Z is (A) a divalent radical, of which all or different portions can be (i) linear, branched, cyclic or bicyclic, (ii) aliphatic or aromatic, and/or (iii) unsaturated, said  
 25 divalent radical being composed of 1-35 carbon atoms together with up to five oxygen, nitrogen, sulfur, phosphorous and/or halogen (such as fluorine, chlorine and/or bromine) atoms; or (B) S, S<sub>2</sub>, SO, SO<sub>2</sub>, O or CO; or (C) a single bond; and  
 (II) each X is independently hydrogen, a halogen (such as fluorine, chlorine and/or  
 30 bromine), a C<sub>1</sub>-C<sub>12</sub> linear or cyclic alkyl, alkoxy, aryl or aryloxy radical, such as methyl, ethyl, isopropyl, cyclopentyl, cyclohexyl, methoxy, ethoxy, benzyl, tolyl, xylyl, phenoxy and/or xylynoxy.

For example, the bridging radical represented by Z in the above formula can be a carbon atom to which is bonded one or more groups such as CH<sub>3</sub>, C<sub>2</sub>H<sub>5</sub>, C<sub>3</sub>H<sub>7</sub>, n-C<sub>3</sub>H<sub>7</sub>, i-C<sub>3</sub>H<sub>7</sub>,  
 35 cyclohexyl, bicyclo[2.2.1]heptyl, benzyl, CF<sub>2</sub>, CF<sub>3</sub>, CCl<sub>3</sub>, CF<sub>2</sub>Cl, CN, (CH<sub>2</sub>)<sub>2</sub>COOCH<sub>3</sub>, or PO(OCH<sub>3</sub>)<sub>2</sub>.

Using a process such as is generally described above, a polycarbonate product can be obtained having a weight average molecular weight, as determined by light scattering or gel permeation chromatography, of 8,000 to 200,000 and preferably 15,000 to 40,000,

although values outside these ranges are permitted as well. Polycarbonate having a weight average molecular weight less than 40,000, preferably less than 35,000, is particularly preferred because of its ease of processing when employed as the dominant matrix resin. Molecular weight can be controlled by addition to the reaction mixture of a chain terminator  
5 which may be selected from monofunctional substances such as phenols, alcohols, amines, imides, carbonic acid chlorides, sulfonic acid chlorides, benzyltriethyl ammonium chloride, or phenylchlorocarbonates. A chain terminator may be added to the reaction mixture before or after a dihydroxy compound is contacted with a carbonate precursor.

A branched rather than linear polycarbonate molecule can be obtained by adding  
10 to the reaction mixture a tri- or polyfunctional monomer such as a tri- or tetrafunctional phenol or carboxylic acid (or a derivative such as an acyl halide or anhydride), a bisphenol containing carboxylic acid side groups, or a nitrogen-containing compound such as cyanuric chloride, or compounds containing a mixture of such groups. Preferred branching agents are trimellitic acid or pyromellitic dianhydride.

15 The preferred process of this invention is that in which an aromatic polycarbonate is prepared. An aromatic polycarbonate is defined herein with reference to the oxygen atoms, of the one or more dihydroxy compounds present in the polycarbonate chain, which are bonded to a carbonyl carbon. In an aromatic polycarbonate, all such oxygen atoms are bridged by a dihydroxy compound residue some portion of which is an aromatic ring.

20 Also included within the term "polycarbonate", as used herein, are various copolycarbonates, certain of which can be prepared by incorporating one or more different dihydroxy compounds into the reaction mixture. This can be accomplished by charging the dihydroxy compounds themselves to the reaction mixture either simultaneously or sequentially. If the dihydroxy compounds are added sequentially or added together but have  
25 different reactivities toward the carbonate precursor, a segmented or block copolycarbonate will typically result. Different dihydroxy compounds with the same reactivity typically yield a random copolycarbonate when reacted together. Alternatively, if oligocarbonates are formed separately from one or more different dihydroxy compounds, the oligocarbonates can then be coupled in a condensation reaction to yield a segmented or block copolycarbonate. When a  
30 dicarboxylic acid (or derivative) or a hydroxycarboxylic acid is used in the reaction mixture, or to form an oligomeric prepolymer, instead of one of the different dihydroxy compounds mentioned above, a poly(ester/carbonate) is obtained.

Copolycarbonates can also be prepared, for example, by reaction of one or more dihydroxy compounds with a carbonate precursor in the presence of a chlorine- or amino-  
35 terminated polysiloxane, with a hydroxy-terminated poly(phenylene oxide) or poly(methyl methacrylate), or with phosphonyl dichloride or an aromatic ester of a phosphonic acid. Siloxane/carbonate block copolymers are discussed in greater detail in Paul, U.S. Pat. No.

4,596,970 and poly(ester/carbonate)s are discussed in greater detail in Swart, U.S. Pat. No. 4,105,533.

The methods generally described above for preparing carbonate polymers suitable for use in the practice of this invention are well known; for example, several methods are discussed in detail in Schnell, USP 3,028,365; Campbell, USP 4,384,108; Glass, USP 4,529,791; and Grigo, USP 4,677,162, each of which is incorporated as a part hereof.

A polyester may be made by the self-esterification of hydroxycarboxylic acids, or direct esterification, which involves the reaction of a diol with a dicarboxylic acid with the resulting elimination of water, giving an  $[-AABB-]$  polyester. Temperatures applied exceed the melting points of the reactants and typically approach the boiling point of the diol being used, and usually range from about 150°C to about 280°C. An excess of the diol is typically used, and once all of the acid has reacted with diol, the excess diol is removed by distillation with the application of additional heat under reduced pressure.

Alternatively, but in like manner, ester-forming derivatives of a dicarboxylic acid can be heated with a diol to obtain polyesters in an ester interchange reaction. Suitable acid derivatives for such purpose are esters, halides, salts or anhydrides of the acid. The ester interchange reaction is typically run in the presence of a diluent, for example, an inert organic solvent such as chloroform or tetrachloroethane, and in the presence of a base, for example a tertiary organic base such as pyridine. Typical catalysts used when ester interchange involves alcoholysis are weak bases such as carbonates or alkoxides of sodium, lithium, zinc, calcium, magnesium or aluminum, whereas catalysts such as antimony oxide, titanium butoxide or sodium acetate are often used when acidolysis occurs in the interchange reaction. Diol derivatives such as an acetate can be used effectively when it is desired to conduct acidolysis.

The molecular weight of polyester can be increased by adding a chain coupling agent, such as diphenyl carbonate, to the melt reaction mixture just prior its completion. Or, to achieve higher weight by solid state polymerization, polyester product of intermediate weight can be heated in a vacuum or stream of inert gas, first to a temperature where it crystallizes and then to a temperature close to its melting point.

Polyesters can also be produced by a ring-opening reaction of cyclic esters or lactones, for which organic tertiary bases and alkali and alkaline earth metals, hydrides and alkoxides can be used as initiators.

Whether a polyester is crystalline or amorphous is typically a function of the symmetry of the starting materials from which it is made. When one or more hydrogens on the diol and/or the diacid (or derivative) which are reacted to form a polyester are replaced by larger radicals such as alkyl or halogen, the intermolecular spacing of the resulting molecules may be disrupted if the presence of the substituent creates asymmetric or irregularly shaped molecules. The component containing the substituent may also be combined into the polyester molecule in random orientation, resulting in structural irregularity in the polymer

chain. Factors which can influence crystallization of ring-containing polyesters are the directionality of the ester groups, the stereochemistry of the rings and variations in symmetry where the rings are bridged. For example, a poly(alkylene isophthalate) crystallizes only with difficulty, and a polyester prepared from phthalic acid typically does not crystallize at all.

- 5 However, where the amount of monomer containing the asymmetry is small in relation to the remainder of the starting materials, the portion of the resulting polyester molecule which suffers from structural irregularity will also be small, and crystallization will typically not be impeded. A crystalline material may be identified by the endotherm it displays on a differential scanning calorimeter. A preferred polyester for use in this invention is a crystalline polyester  
10 having a melting point of 254-260°C.

- Suitable reactants for making the polyester used in this invention, in addition to hydroxycarboxylic acids, are diols and dicarboxylic acids either or both of which can be aliphatic or aromatic. A polyester which is a poly(alkylene alkanedicarboxylate), a poly(alkylene phenylenedicarboxylate), a poly(phenylene alkanedicarboxylate), or a poly(phenylene  
15 phenylenedicarboxylate) is therefore appropriate for use herein. Alkyl portions of the polymer chain can be substituted with, for example, halogens, alkoxy groups or alkyl side chains and can contain divalent heteroatomic groups (such as -O-, -S- or -SO<sub>2</sub>-) in the paraffinic segment of the chain. The chain can also contain unsaturation and non-aromatic rings. Aromatic rings can contain substituents such as halogens, alkoxy or alkyl groups, and can be joined to the polymer  
20 backbone in any ring position and directly to the alcohol or acid functionality or to intervening atoms.

- Typical alkylene diols used in ester formation are the C<sub>2</sub>-C<sub>10</sub> glycols, such as ethylene-, propylene-, and butylene glycol. Alkanedicarboxylic acids frequently used are oxalic acid, adipic acid and sebacic acid. Diols which contain rings can be, for example, a 1,4-  
25 cyclohexylenyl glycol or a 1,4-cyclohexane-dimethylene glycol, resorcinol, hydroquinone, 4,4'-thiodiphenol, bis-(4-hydroxyphenyl)sulfone, a dihydroxynaphthalene, a xylylene diol, or can be one of the many bisphenols such as 2,2-bis-(4-hydroxyphenyl)propane. Aromatic diacids include, for example, terephthalic acid, isophthalic acid, naphthalenedicarboxylic acid, diphenyletherdicarboxylic acid, diphenyldicarboxylic acid, diphenylsulfonedicarboxylic acid,  
30 diphenoxyethanedicarboxylic acid.

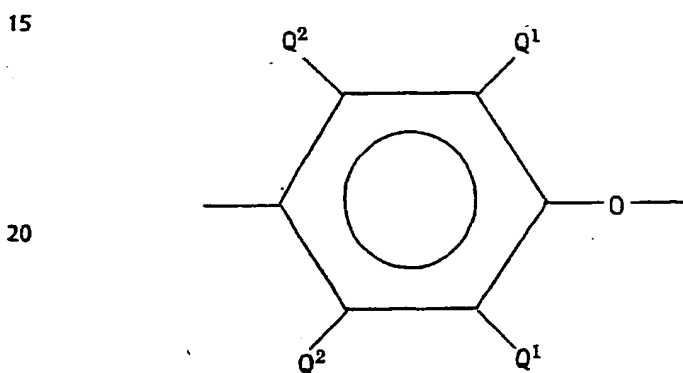
- In addition to polyesters formed from one diol and one diacid only, the term "polyester" as used herein includes random, patterned or block copolyesters, for example those formed from two or more different diols and/or two or more different diacids, and/or from other divalent heteroatomic groups. Mixtures of such copolyesters, mixtures of polyesters  
35 derived from one diol and diacid only, and mixtures of members from both of such groups, are also all suitable for use in this invention, and are all included in the term "polyester". For example, use of cyclohexanedimethylol together with ethylene glycol in esterification with terephthalic acid forms a clear, amorphous copolyester ("PETG") of particular interest. Also

contemplated are PCTG; liquid crystalline polyesters derived from mixtures of 4-hydroxybenzoic acid and 2-hydroxy-6-naphthoic acid; or mixtures of terephthalic acid, 4-hydroxybenzoic acid and ethylene glycol; or mixtures of terephthalic acid, 4-hydroxybenzoic acid and 4,4'-dihydroxybiphenyl.

5 Aromatic polyesters, those prepared from an aromatic diacid, such as the poly(alkylene phenylenedicarboxylates) polyethylene terephthalate and polybutylene terephthalate, or mixtures thereof, are particularly useful in this invention.

Methods and materials useful for the production of polyesters, as described above, are discussed in greater detail in Whinfield, US Pat. No. 2,465,319, Pengilly, US Pat. No. 3,047,539 and Russell, US Pat. No. 3,756,986, each of which is incorporated herein by reference.

10 A poly(phenylene ether) [also known as a poly(phenylene oxide)] is a polymer comprising a plurality of structural units described generally by the formula



In each of said units independently, each Q¹ is independently hydrogen, halogen, primary or secondary

C<sub>1</sub> - C<sub>8</sub> lower alkyl, phenyl, haloalkyl, aminoalkyl, hydrocarboxy, or haloalkylhydrocarboxy  
 30 wherein at least two carbon atoms separate the halogen and oxygen atoms; and each Q² is independently hydrogen, halogen, primary or secondary C<sub>1</sub> - C<sub>8</sub> lower alkyl, phenyl, haloalkyl, hydrocarboxy or haloalkylhydrocarboxy as defined for Q¹. Examples of suitable primary lower alkyl groups are methyl, ethyl, n-propyl, n-butyl, isobutyl, n-amyl, isoamyl, 2-methylbutyl, n-hexyl, 2,3-dimethylbutyl, 2-, 3- or 4-methylpentyl and the corresponding heptyl groups.  
 35 Examples of secondary lower alkyl groups are isopropyl, sec-butyl and 3-pentyl. It is preferred that any alkyl radicals are straight chain rather than branched. Most often, each Q¹ is alkyl or phenyl, especially C<sub>1-4</sub> alkyl, and each Q² is hydrogen.

Both homopolymer and copolymer poly(phenylene ether)s are included, as well as mixtures or blends thereof. Suitable homopolymers are those containing, for example, 2,6-dimethyl-1,4-phenylene ether units. Suitable copolymers include random copolymers containing such units in combination with, for example, 2,3,6-trimethyl-1,4-phenylene ether units.

Also included are poly(phenylene ether)s containing moieties which modify properties such as molecular weight, melt viscosity and/or impact strength. Such polymers may be prepared by copolymerizing with or grafting onto the poly(phenylene ether), in known manner, such vinyl monomers as vinyl nitrile compounds (e.g. acrylonitrile) and vinyl aromatic compounds (e.g., styrene), or such polymers as polystyrenes and elastomers. The product typically contains both grafted and ungrafted moieties. Other suitable polymers are the coupled poly(phenylene ether)s in which the coupling agent is reacted, in known manner, with the hydroxy groups of two poly(phenylene ether) chains to produce a higher molecular weight polymer containing the reaction product of the hydroxy groups and the coupling agent. Illustrative coupling agents are low molecular weight polycarbonates, quinones, heterocycles, formals and poly(phenylene sulfide)s. For example, poly(phenylene ether)/polycarbonate copolymers are known and are discussed in U.S. Pat. No. 5,010,143, which is incorporated herein.

The poly(phenylene ether) typically has a number average molecular weight within the range of about 3,000-40,000, and a weight average molecular weight within the range of about 20,000-80,000, as determined by gel permeation chromatography. Its intrinsic viscosity is typically in the range of about 0.15-0.6, and preferably at least 0.25, dL/g, as measured in chloroform at 25°C. However, values outside these ranges are permitted as well.

The poly(phenylene ether)s are typically prepared by the oxidative coupling of at least one corresponding monohydroxyaromatic compound. Particularly useful and readily available monohydroxyaromatic compounds are 2,6-xylenol (wherein each Q<sup>1</sup> is methyl and each Q<sup>2</sup> is hydrogen), whereupon the polymer may be characterized as a poly(2,6-dimethyl-1,4-phenylene ether), and 2,3,6-trimethylphenol (wherein each Q<sup>1</sup> and one Q<sup>2</sup> is methyl and the other Q<sup>2</sup> is hydrogen).

A variety of catalyst systems are known for the preparation of poly(phenylene ether)s by oxidative coupling. For the most part, they contain at least one heavy metal compound such as a copper, manganese or cobalt compound, usually in combination with various other materials.

A first class of preferred catalyst systems consists of those containing a copper compound, such as are disclosed, for example, in U.S. Pat. Nos. 3,306,874, 3,306,875, 3,914,266 and 4,028,341, each of which is incorporated herein. They are usually combinations of cuprous or cupric ions, halide (i.e., chloride, bromide or iodide) ions and at least one amine.



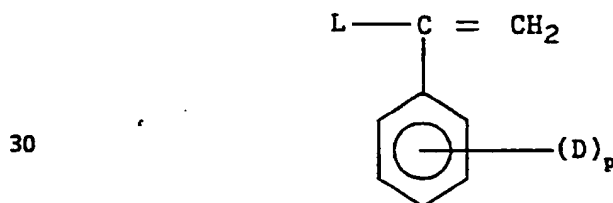
Catalyst systems containing manganese compounds constitute a second preferred class. They are generally alkaline systems in which divalent manganese is combined with such anions as halide, alkoxide or phenoxide. Most often, the manganese is present as a complex with one or more complexing and/or chelating agents such as dialkylamines, alkanolamines, alkylenediamines, *o*-hydroxyaromatic aldehydes, *o*-hydroxyazo compounds, *ω*-hydroxyoximes (monomeric and polymeric), *o*-hydroxyaryl oximes and  $\beta$ -diketones. Also useful are known cobalt-containing catalyst systems.

Poly(phenylene ether)s, as described above, are discussed in greater detail in U.S. Pat. No. 4,866,130, which is incorporated herein in its entirety.

A poly(phenylene ether) blend may be prepared by blending a poly(phenylene ether) with polystyrene, a vinyl aromatic copolymer, and/or with other non-styrenic polymers as specified below. The poly(phenylene ether) blend made up of about 20 to about 99 parts poly(phenylene ether), and preferably about 30 to 90 parts poly(phenylene ether), by weight, with the balance being made up of polystyrene, a vinyl aromatic copolymer, and/or the non-styrenic polymers, in addition to additives such as dyes and pigments. A preferred formulation of the poly(phenylene ether) blend contains about 30 to about 85 weight parts poly(phenylene ether), about 15 to about 70 weight parts selected from one or more of the following: polystyrene, high impact polystyrene, styrene/butadiene/styrene and/or styrene/ethylene-butylene/styrene block copolymer, and about 0.1 to about 20 weight parts pigments and/or dyes.

A polystyrene includes polymers prepared by bulk, suspension or emulsion polymerization which contain at least 25 percent by weight structural units derived from a monomer described generally by the formula

25



wherein L is hydrogen,  $\text{C}_{1-8}$  lower alkyl or halogen, D is vinyl, halogen or lower alkyl, and p is from 0 to 5. These resins include homopolymers of styrene, chlorostyrene and vinyltoluene; random copolymers of styrene with one or more monomers illustrated by acrylonitrile, an alkyl acrylate, butadiene,  $\alpha$ -methylstyrene, ethylvinylbenzene, divinylbenzene, maleic anhydride and phenyl maleimide; an ethylene/propylene/diene copolymer grafted with acrylonitrile

and/or styrene; and rubber modified polystyrenes comprising blends and grafts, wherein the rubber is a polybutadiene or a rubbery copolymer of about 70-98 percent styrene and about 2-30 percent diene monomer. A polystyrene as described above may also be rubber-modified by blending it with a hydrogenated or unhydrogenated vinyl aromatic/diene block copolymer, containing at least thirty percent vinyl aromatic compound by weight, which yields a high impact polystyrene ("HIPS").

The poly(phenylene ether) blend in the compositions of this invention may also be a blend of poly(phenylene ether) with a copolymer prepared from a vinyl aromatic compound and one or more copolymerizable, ethylenically unsaturated monomers.

Appropriate copolymerizable, ethylenically unsaturated monomers for preparation of such a vinyl aromatic copolymer may be described in general as  $R_2-C=C-R_2$ , where each R is independently

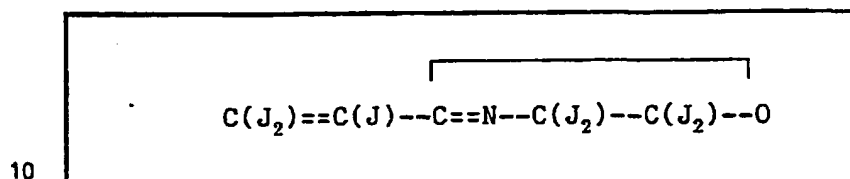
- (1) hydrogen; (2) a halogen such as F, Cl, Br or I; (3) -OH; (4) -CO<sub>2</sub>H; (5) -SH; (6) -CN; (7) -NO<sub>2</sub>; or (8) -C<sub>1</sub>-C<sub>8</sub>Z; (9) -C(O)Z; (10) -CO<sub>2</sub>Z; (11) -CO<sub>2</sub>NZ<sub>2</sub>; (12) -OZ; (13) -SZ; (14) -SOZ; (15) -SO<sub>2</sub>Z; (16) -NZ<sub>2</sub>; or (17) -PZ<sub>2</sub> (where Z is H, halogen, O, -OH, -CO<sub>2</sub>H, -SH, -CN, -NO<sub>2</sub> or an epoxide ring; or a C<sub>1</sub> - C<sub>10</sub> linear or branched, saturated or unsaturated, alkyl radical or a C<sub>6</sub> - C<sub>14</sub> aryl radical substituted with halogen, -OH, -CO<sub>2</sub>H, -SH, -CN, -NO<sub>2</sub> or an epoxide ring); or
- (b) a C<sub>1</sub> - C<sub>10</sub> linear or branched, saturated or unsaturated, alkyl radical optionally substituted with, or interruptible with, a phenyl radical or one or more members of group (a); or
- (c) a phenyl or naphthyl radical, each independently optionally substituted with a C<sub>1</sub> - C<sub>6</sub> linear or branched, saturated or unsaturated, alkyl radical or one or more members of group (a).

However, it is not required that all of the substituents named above as being represented by R be utilized, and any one or more of such substituents, or sub-components thereof, may be omitted as desired in the practice of this invention.. The vinyl aromatic copolymer may be a random, alternate, block or grafted copolymer, and a mixture of more than one vinyl aromatic copolymer may be used as well.

Ethylenically unsaturated monomers of particular interest for copolymerization with a vinyl aromatic compound include a vinyl nitrile compound, a diene, an alkyl or aryl acrylate or methacrylate, glycidyl methacrylate, an alkyl or aryl maleate or fumarate, maleic anhydride, an alkyl or aryl maleimide, ethylene/propylene/diene copolymer, and an oxazoline compound.

In addition to other particular species of various ethylenically unsaturated monomers which are noted below in the discussion of producing acrylonitrile/butadiene/styrene copolymer ("ABS"), the category of vinyl aromatic compounds

includes styrene and substituted styrenes; vinyl nitrile compounds include acrylonitrile and substituted acrylonitriles; alkyl acrylates and methacrylates include  $C_1 - C_{10}$  acrylates and methacrylates; alkyl or aryl maleimide compounds include the reaction product of a  $C_1 - C_{10}$  alkyl or  $C_6 - C_{14}$  aryl primary amine and maleic anhydride; and an oxazoline compound includes  
 5 those of the general formula



where each J is independently hydrogen, halogen, a  $C_1 - C_{10}$  alkyl radical or a  $C_6 - C_{14}$  aryl radical.

One example of a vinyl aromatic copolymer useful for incorporation into the poly(phenylene ether) blend is a vinyl aromatic/vinyl nitrile copolymer such as  
 15 styrene/acrylonitrile copolymer ("SAN"). SAN which has been rubber modified is also suitable for use as a blend material, and an example of a rubber modified SAN is a vinyl nitrile/diene/vinyl aromatic copolymer such as ABS.

ABS, an elastomeric-thermoplastic composite, is typically formed by the grafting of an SAN copolymer onto a polybutadiene substrate latex. The polybutadiene forms particles  
 20 of rubber - the elastomeric component - which are dispersed as a discrete phase in a thermoplastic matrix formed by the SAN. The rubber content of a rubber-modified styrene/acrylonitrile copolymer employed in the compositions of this invention can be up to 80 percent, but is preferably less than 40 percent.

One method for making a vinyl aromatic copolymer is emulsion polymerization.  
 25 For example, when ABS is made by emulsion polymerization, a rubber substrate latex is produced in an aqueous emulsion by a polymerization, which can be initiated by organic peroxides, persulfates or redox systems, of 1,3-butadiene alone or in combination with other diene monomers such as isoprene, 2,3-dimethyl butadiene-1,3 or piperylene, or a combination of two or more of these and a lesser amount of one or more of the following: vinyl aromatic  
 30 monomers such as styrene, alpha-alkyl styrene, p-methoxy styrene, p-chloro styrene, dichloro styrene or vinyl naphthalene; vinyl nitrile monomers such as acrylonitrile, methacrylonitrile, ethacrylonitrile or alphachloro acrylonitrile; alkyl acrylates and methacrylates such as methyl acrylate, propyl acrylate, butyl acrylate, octyl acrylate, methyl alpha-chloro acrylate, methyl methacrylate, ethyl methacrylate or isobutyl methacrylate; methacrylamide or acrylamide,  
 35 N,N-diethyl acrylamide; aliphatic or aromatic maleimides such as N-phenyl maleimide; diethylchloromaleate; diethyl fumarate; vinylidene chloride; methyl vinyl ketone or methyl isopropenyl ketone; vinyl pyridines; vinyl furan; vinyl carbazole; isobutylene or ethylene;

and the like. It is preferred that, in the preparation of the rubber latex, the proportion of butadiene to other monomers in the substrate latex be in the range of about 2/1 to about 15/1.

After formation of the rubber latex substrate, it is subjected to further aqueous emulsion polymerization with styrene and acrylonitrile monomers, wherein the concentration of styrene is usually about 1.5 to 3.5 times that of acrylonitrile. However, other monomers (including various vinyl aromatic or vinyl nitrile compounds) such as methacrylonitrile, divinylbenzene,  $\alpha$ -methyl styrene, p-methyl styrene, methyl methacrylate, N-phenyl maleimide, chlorinated and brominated styrenes, and methyl-, ethyl- or n-butylacrylate, or mixtures thereof, may also be used in conjunction with styrene and acrylonitrile as the grafting monomers.

Organic peroxides, azo compounds, persulfates, or redox systems are usually used to initiate polymerization. SAN is formed, some of which is grafted to the rubber latex substrate, and some of which is free. The latex containing both the grafted rubber and the free SAN is then mixed with a coagulant solution, heated and agitated to produce discrete particles of ABS resin. The slurry containing those particles is dewatered in a centrifuge, and the resin is dried. Methods for making ABS resin by emulsion polymerization, as described above, are discussed in greater detail in Childers, USP 2,820,773 and Calvert, USP 3,238,275, each being hereby incorporated as a part hereof.

Another method for making a vinyl aromatic copolymer is suspension polymerization. For example, when ABS is made by suspension polymerization, a pre-formed elastomeric (rubber) component, usually a polybutadiene or a butadiene/styrene copolymer, is dissolved in a mixture of styrene and acrylonitrile. The rubber component may be one of the several mentioned above with respect to emulsion polymerization of ABS, or may be a diene such as polyisoprene, polycyclopentadiene, natural rubber, chlorinated rubber or copolymers of butadiene with isobutylene.

The preferred ratio of styrene to acrylonitrile in the styrene-acrylonitrile solution is about 99/1 to about 60/40, and in the preferred recipe the rubber component constitutes from about 4% to less than about 40% of the product. As with the emulsion process described above, numerous other vinyl aromatic compounds will function in a manner equivalent to that of styrene, to-wit:  $\alpha$ -methyl styrene, vinyl-toluene, vinylxylene, vinyl ethyl benzene or vinylchloro benzene. Methacrylonitrile is but one of many other vinyl nitrile monomers which will serve in the place of, or in conjunction with, acrylonitrile.

The rubber component, monomers and initiator are charged to the reaction vessel and polymerization ensues until a conversion rate of about 15% to about 30% is reached, resulting in the production of a prepolymer. Phase inversion occurs, and the rubber precipitates from solution and becomes the discontinuous phase dispersed as particles ranging from 0.1 to 5  $\mu$ m in size. The prepolymer is then placed in a suspension reactor in an aqueous solution containing a suspending agent, initiator and chain transfer agent. Typical suspending

agents are carboxymethyl cellulose, polyvinyl alcohol, and polyglycol ethers. Typical initiators for the polymerization which occurs during suspension are t-butyl perbenzoate, di-t-butyl peroxide, or t-butylperoxy isopropyl carbonate. Agitation of the solution completes the polymerization. The process is completed by dewatering the slurry in a centrifuge, and  
5 moisture content is further reduced by flash drying. Manufacture of ABS by the suspension process, as described above, is discussed in greater detail in Carrock, USP 3,515,692 and Ackerman, USP 4,151,128, each being hereby incorporated as a part hereof.

A third method for production of a vinyl aromatic copolymer is bulk or mass polymerization. For example, when ABS is made by bulk or mass polymerization, it is formed  
10 by dissolving an elastomeric (rubber) component in the monomer mix, which contains styrene, acrylonitrile, an initiator and, frequently, a chain transfer agent such as a mercaptan or a terpinolene. The reaction can, however, be thermally initiated. The styrene and acrylonitrile monomers polymerize, some grafting to the rubber component, but most forming a monomer-polymer solution. As the relative volume of the monomer-SAN polymer phase increases,  
15 discrete rubber particles become dispersed in the matrix resulting from the monomer-SAN polymer phase. The rubber particles are stabilized by being grafted to SAN polymers at the interface between the particles and the SAN polymer matrix. Additional stabilization is furnished when monomer becomes occluded, and polymerizes, within the rubber particles. Because polymerization occurs completely within a monomer/polymer medium, viscosity  
20 increases as conversion increases. To allow continued agitation of the reaction mixture despite such increasing viscosity, diluents such as methyl ethyl ketone and ethylbenzene are added to the reactor. Upon the completion of polymerization, the melt is devolatilized using equipment such as a devolatilizing extruder or a flash evaporator, and vacuum is applied to remove unreacted monomers and diluents.

As is true of ABS made by the emulsion or suspension method, numerous  
25 substances can be used in the bulk method in place of, or conjunction with, styrene, examples of such substances being vinyl aromatic compounds as follows: alpha-methylstyrene, alpha-ethylstyrene, alpha-methylvinyltoluene; ring-substituted alkyl styrenes, e.g. vinyl toluene, o-ethylstyrene, p-ethylstyrene, 2,4-dimethylstyrene; ring-substituted halostyrenes, e.g., o-  
30 chlorostyrene, p-chlorostyrene, o-bromostyrene, 2,4-dichlorostyrene; ring-alkyl, ring-halo-substituted styrenes, e.g. 2-chloro-4-methylstyrene and 2,6-dichloro-4-methylstyrene. Also useful are methacrylates such as methyl methacrylate; maleic acid and its esters and anhydrides; aliphatic or aromatic maleimides such as N-phenyl maleimide; and mixtures of any of the foregoing. Methacrylonitrile can also be used in combination with acrylonitrile.  
35 Bulk methods for the preparation of ABS, as described above, are discussed in greater detail in Kruse, USP 4,187,260, Simon, USP 4,252,911 and Weber, USP 4,526,926, each being hereby incorporated as a part hereof.

AES (acrylonitrile/EPDM/styrene) copolymer is a vinyl aromatic copolymer which is obtained when styrene/acrylonitrile copolymer is rubber-modified by grafting SAN to a substrate made up of an EPDM (ethylene/propylene/non-conjugated diene) rubber. AES copolymers are discussed in greater detail in Henton, USP 4,766,175, which is incorporated as a part hereof. SAN can also be crosslinked to an acrylate elastomer to form a vinyl aromatic copolymer, as in the case of an ASA (acrylonitrile/styrene/acrylate) copolymer, which is discussed in greater detail in Yu, USP 3,944,631, which is also incorporated as a part hereof. Other vinyl aromatic copolymers of particular interest include aryl maleimide/vinyl nitrile/diene/vinyl aromatic copolymer, vinyl aromatic/maleic anhydride copolymer, alkyl methacrylate/vinyl aromatic/vinyl nitrile copolymer, vinyl aromatic/alkyl methacrylate copolymer, vinyl aromatic/alkyl methacrylate/glycidyl methacrylate copolymer, vinyl aromatic/glycidyl methacrylate copolymer, styrene/butyl acrylate copolymer, methyl methacrylate/acrylonitrile/butadiene/styrene copolymer and phenyl maleimide/acrylonitrile/butadiene/styrene copolymer.

Yet another form which a vinyl aromatic copolymer can take, for blending with poly(phenylene ether), is a block copolymer which can be either linear, branched, radial or teleblock, and can be either a di-block ("A-B") copolymer, tri-block ("A-B-A") copolymer, or radial teleblock copolymer with or without tapered sections, i.e. portions of the polymer where the monomers alternate or are in random order close to the point of transition between the A and B blocks. The A portion is made by polymerizing one or more vinyl aromatic hydrocarbon monomers, and has an average molecular weight of about 4,000 to about 115,000, and a weight preferably of about 8,000 to about 60,000. The B portion of the block copolymer results from polymerizing a diene and has a molecular weight of about 20,000 to about 450,000, and a weight preferably of about 50,000 to about 300,000. In the A-B di-block copolymer, each block, A or B, can vary from 10-90% of the total weight of the copolymer. In the A-B-A tri-block copolymer, the A end groups typically constitute about 2 wt% to about 55 wt% of the whole block copolymer, and preferably are between 5 wt% and 45 wt% of the whole block copolymer.

The A block of the block copolymer has properties characteristic of thermoplastic substances in that it has the stability necessary for processing at elevated temperatures and yet possesses good strength below the temperature at which it softens. The A block is polymerized predominantly from vinyl aromatic hydrocarbons, and substituted derivatives thereof wherein the aromatic moiety can be either mono- or polycyclic. Monomers from which the thermoplastic end blocks can be formed are, for example, styrene and substituted derivatives thereof such as  $\alpha$ -methyl styrene, vinyl xylene, vinyl naphthalene, and the like, and mixtures of two or more thereof. Other vinyl monomers such as methyl acrylate, methyl methacrylate, phenyl maleimide, acrylonitrile or vinyl pyridine may be used in the formation of the A block together with the aromatic monomers. The polymerization can be initiated by lithium metal,

or alkyl- or aryl lithium compounds such as butyl lithium or isoamyl lithium. Polymerization is normally conducted at temperatures ranging from about -20°C to about 100°C.

The B block of the copolymer can be formed, for example, simply by injecting suitable monomer into the reaction vessel and displacing the lithium radical from the just-  
5 polymerized A block, which then acts as an initiator because it is still charged. The B block is formed predominantly from substituted or unsubstituted C<sub>2</sub>-C<sub>10</sub> dienes, particularly conjugated dienes such as butadiene or isoprene. Other diene, vinyl or olefinic monomers such as chloroprene, 1,4-pentadiene, isobutylene, ethylene or vinyl chloride may be used in the formation of the B block provided that they are present at a level low enough to not alter the  
10 fundamental olefinic character of the B block. The B block will be characterized by elastomeric properties which allow it to absorb and dissipate an applied stress and then regain its shape.

In the A-B-A tri-block copolymer, the second end block A can be formed in a manner similar to the first, by injecting appropriate vinyl aromatic monomer into the reaction vessel. Alternatively, a bivalent lithium initiator can be used, which, when brought together  
15 with the diene monomer under the same conditions described above, will form an elastomeric mid block B which carries a charge at each end. Then, upon addition of vinyl aromatic monomer to the reaction mixture, a thermoplastic end block A will form on both ends of the mid block B, yielding a thermoplastic elastomeric A-B-A copolymer.

To reduce oxidative and thermal instability, the block copolymers used herein can  
20 also desirably be hydrogenated to reduce the degree of unsaturation on the polymer chain and on the pendant aromatic rings. The block copolymer may be selectively hydrogenated by hydrogenating only the elastomeric block B. Typical hydrogenation catalysts utilized are Raney nickel, molybdenum sulfide, finely divided palladium and platinum oxide. The hydrogenation reaction is typically run at 75-450°F and at 100-1,000 psig for 10-25 hours.

The most preferred vinyl aromatic block copolymers are vinyl  
25 aromatic/conjugated diene block copolymers formed from styrene and butadiene or styrene and isoprene. When the styrene/butadiene copolymers are hydrogenated, they are frequently represented as styrene/(ethylene/butylene) copolymer in the di-block form, or as styrene/(ethylene/butylene)/styrene copolymer in the tri-block form. When the  
30 styrene/isoprene copolymers are hydrogenated, they are frequently represented as styrene/(ethylene/propylene) copolymer in the di-block form, or as styrene/(ethylene/propylene)/styrene copolymer in the tri-block form. The vinyl aromatic/diene block copolymers described above are discussed in greater detail in Holden, USP 3,265,766; Haefele, USP 3,333,024; Wald, USP 3,595,942; and Witsiepe, USP 3,651,014, each of which is  
35 incorporated herein.

Whether a poly(phenylene ether) blend ("PPE Blend"), poly(phenylene ether) as a neat polymer, or a mixture of the two, is combined with the matrix resin, it is preferred, but not required, that the poly(phenylene ether) be immiscible in the matrix resin such that the

poly(phenylene ether), or the poly(phenylene ether) which contains a miscible portion of a vinyl aromatic copolymer alloy component in a PPE Blend, is dispersed within the matrix resin as particles on the order of about 0.3-10 microns, and more preferably about 0.3-6 microns. The immiscibility of two or more polymers may be determined visually by examination of a transmission electron micrograph of a composition containing them, or by determining whether such composition containing them exhibits more than one glass transition temperature ( $T_g$ ).  $T_g$  may be determined, for example, by calorimetry. Particle size may also be determined visually by examination of a transmission electron micrograph.

In a particularly preferred embodiment, when a vinyl aromatic block copolymer is blended with a poly(phenylene ether) to form a PPE Blend, the vinyl aromatic phase of the block copolymer, although distinguishable from the poly(phenylene ether) phase, resides within the poly(phenylene ether) phase because of the miscibility of the vinyl aromatic block with poly(phenylene ether).

A PPE Blend represents a poly(phenylene ether) concentrate because poly(phenylene ether) is typically present in the PPE Blend at a higher level of content than it will be in the final composition of which the PPE Blend itself becomes a part. The desired level of content of poly(phenylene ether) in a composition of this invention is reached by diluting the amount of poly(phenylene ether) in the concentrate by the admixture of other components with the PPE Blend in the final composition.

The presence of polystyrene and/or a vinyl aromatic copolymer in a PPE Blend reduces the processing temperature and/or viscosity of the poly(phenylene ether) to a level which makes it possible, if desired, to add a poly(phenylene ether) concentrate to a composition hereof directly at a molding machine rather than in a pre-molding extruded mixture. A composition of blend components which is to be molded is typically first processed by melt mixing all of the components together in an extruder. The resulting mixture is then re-melted in a molding machine for molding. However, because polystyrene and/or a vinyl aromatic copolymer in a PPE Blend imparts to the poly(phenylene ether) concentrate a processing temperature and/or viscosity which are lower than that of poly(phenylene ether) by itself, the concentrate may be added to the final composition directly at the molding machine rather than in the pre-molding extruded mixture.

Non-styrenic polymers which can be blended with poly(phenylene ether), polystyrene and/or a vinyl aromatic copolymer as a part of a poly(phenylene ether) blend are polyamide, polycarbonate, polyester and an acrylate and/or methacrylate polymer, or a mixture thereof. Polycarbonate and polyester are described above.

The polyamides suitable for use in this invention can be produced by the condensation of bifunctional monomers, typically those containing acid and amine functionalities, where the monomers have either the same or different functional groups. For example, if hexamethylenediamine is reacted with adipic acid, an -[AABB]- type polyamide is



obtained wherein the diamine and diacid units alternate. However, when a monomer such as an amino acid or a cyclic lactam is self-polymerized, an  $[-AB-]$  type polyamide results from a regular head-to-tail polymerization, similar to an addition mechanism. For example, when nylon-6 is made, heat is applied to raise the temperature of the caprolactam to 240-280°C, and  
5 catalysts such as water and phosphoric acid are added to the system. Hydrolysis ensues, the ring opens and polymerization takes place while unreacted monomer is removed from the system and recycled. Polycondensation and growth of the polymer chain results from the removal of water from the system.

The polyamides suitable for use herein also include those wherein two or more  
10 different diamines, and/or different diacids and/or different amino acids are polymerized together to form a random or block co-polyamide. The carbon chain between the functional groups may be linear or branched aliphatic, alicyclic or aromatic hydrocarbons. The chains may also contain hetero atoms such as oxygen, sulfur or nitrogen. Also suitable for use herein are block or random copolymers, such as those resulting, for example, from melt mixing two or  
15 more different polyamides, from reaction of a diamine or diacid monomer that contains an amide linkage with another diamine or diacid, or from reaction of a diisocyanate with a dicarboxylic acid.

Polyamides are most often prepared by direct amidation in which the amine group of a diamine or an amino acid bonds to the carboxyl of a diacid with the accompanying  
20 elimination of water. Derivatives of the acid function, such as an ester, acyl halide or amide, may be used as an alternative source of the carboxyl functionality, in which case the by-product is an alcohol, a hydrogen halide or ammonia, respectively. For example, when an acid chloride is used, the diacid chloride in a water-immiscible solvent can be added to an aqueous solution of the diamine, an inorganic base and a surface active agent, and interfacial polymerization  
25 occurs in the organic layer. When polymerization occurs in solution, an organic base such as pyridine is used as the acid acceptor. Formation of polyamides can also occur by ring-opening polymerization of a caprolactam, such as when nylon-6 is made from  $\epsilon$ -caprolactam. Such a reaction can be run at high temperature, in which case water or an amino acid is used as the initiator, or if it is run at low temperature, the ring opening is effected by a strong base, such as  
30 NaOH, usually with the addition of an acylating cocatalyst such as acetic anhydride.

Polyamides as described above, and methods for preparing same, are discussed in greater detail in U.S. Pats. No. 2,071,253, 2,130,523 and 2,130,948, each of which is incorporated as a part hereof.

An acrylate polymer is defined as a polymer prepared by homopolymerization of  
35 an alkyl acrylate or an alkyl methacrylate or by copolymerization of a mixture of the two; and includes a mixture of any such homopolymers or copolymers.

An alkyl acrylate or methacrylate can be prepared, for example, by reaction of an alkyl alcohol or diazoalkane with acrylic or methacrylic acid. Acrylic acid is prepared by the

vapor phase oxidation of propylene. The acrylic acid/alcohol esterification reaction can be run at about 80°C using an acid catalyst such as  $H_2SO_4$ . Methacrylic acid may be prepared by the oxidation of isobutylene or t-butyl alcohol. A methacrylate may also be prepared by reacting acetone cyanohydrin with an excess of concentrated sulfuric acid to form methacrylamide sulfate, which, when then reacted with an alcohol, yields a methacrylate. A  $C_1 - C_{10}$  acrylate or methacrylate may be used for polymer preparation herein, with  $C_1 - C_6$  acrylate or methacrylate being preferred, and  $C_1 - C_4$  being more preferred.

The acrylate polymer used in the compositions of this invention can be prepared in a polymerization reaction initiated by free radical initiators such as azo compounds or peroxides, preferably in the absence of oxygen. Methacrylate monomers are most often polymerized in bulk, but this method has little application for acrylate monomers. Acrylate and methacrylate monomers may be polymerized in an organic solution, using, for example, an aromatic hydrocarbon, ester, ketone or chlorohydrocarbon (such as toluene, chlorobenzene or 3-pentanone) as the solvent. A chain transfer agent such as a thiol may be used to control molecular weight. Polymerization can also occur in an aqueous emulsion in which an anionic surfactant, such as an alkylarene sulfate or phosphate, a nonionic surfactant, such as an alkyl or aryl polyoxyethylene, or a cationic surfactant is used. Suspension polymerization is used primarily for methacrylates and involves suspending in water 0.1-5 mm droplets of monomer which are stabilized by a protective colloid such as cellulose, poly(vinyl alcohol), gelatin or talc. The initiator should be soluble in the monomer but not in water. Acrylates and methacrylates can also be polymerized in a non-aqueous dispersion using an organic diluent such as hexane or methanol.

When an acrylate and a methacrylate are copolymerized, the acrylate, each can be used in the mix of reactants from which the copolymer results in an amount of up to about 99.0 parts by weight, based on the total weight of the copolymer. When the acrylate polymer in a poly(phenylene ether) blend takes the form of a copolymer of an acrylate and a methacrylate, the copolymer may be a random, alternate, block or grafted copolymer.

An acrylate copolymer may be prepared using the methods described above by copolymerization of an alkyl acrylate, an alkyl methacrylate, or a mixture thereof, with one or more other copolymerizable, ethylenically unsaturated monomers. The term "acrylate copolymer" as used herein is not therefore intended to limit the content of such copolymer, which, as described in the preceding sentence, includes copolymers which can contain methacrylates in addition to other copolymerizable monomers, and which are copolymers by reason of being prepared from more than one monomer.

Virtually any ethylenically unsaturated monomer capable of homopolymerization under the conditions described above can be copolymerized with an acrylate, a methacrylate, or both. Representative monomers suitable for such copolymerization to form component (a) can be described as  $R_1-C=C-R_2$ , where each R is independently

- (a) (1) hydrogen; (2) a halogen such as F, Cl, Br or I; (3) -OH; (4) -CO<sub>2</sub>H; (5) -SH; (6) -CN; (7) -NO<sub>2</sub>; or (8) -C<sub>1</sub>-C<sub>8</sub>Z; (9) -C(O)Z; (10) -CO<sub>2</sub>Z; (11) -CO<sub>2</sub>NZ<sub>2</sub>; (12) -OZ; (13) -SZ; (14) -SOZ; (15) -SO<sub>2</sub>Z; (16) -NZ<sub>2</sub>; or (17) -PZ<sub>3</sub> (where Z is H, halogen, O, -OH, -CO<sub>2</sub>H, -SH, -CN, -NO<sub>2</sub> or an epoxide ring; or a C<sub>1</sub> - C<sub>10</sub> linear or branched, saturated or unsaturated, alkyl radical or a C<sub>6</sub> - C<sub>14</sub> aryl radical substituted with halogen, -OH, -CO<sub>2</sub>H, -SH, -CN, -NO<sub>2</sub> or an epoxide ring); or
- (b) a C<sub>1</sub> - C<sub>10</sub> linear or branched, saturated or unsaturated, alkyl radical optionally substituted with, or interruptible with, a phenyl radical or one or more members of group (a); or
- (c) a phenyl or naphthyl radical, each independently optionally substituted with a C<sub>1</sub> - C<sub>6</sub> linear or branched, saturated or unsaturated, alkyl radical or one or more members of group (a).

However, it is not required that all of the substituents named above as being represented by R be utilized, and any one or more of such substituents, or sub-components thereof, may be omitted as desired in the practice of this invention.

Monomers of particular interest for copolymerization with an acrylate and/or a methacrylate include phenyl maleimide, styrene or a C<sub>1</sub>-C<sub>10</sub> alkyl or halogen substituted styrene, acrylonitrile or a C<sub>1</sub>-C<sub>10</sub> alkyl or halogen substituted acrylonitrile, maleic anhydride, a C<sub>1</sub>-C<sub>12</sub> diene, or a mixture thereof.

When an acrylate and/or a methacrylate are copolymerized with one or more other ethylenically unsaturated monomers, the acrylate and/or the methacrylate, and each of the ethylenically unsaturated monomers can each be used in the mix of reactants from which the copolymer results in an amount of up to about 99.0 parts by weight, based on the total weight of the copolymer. The acrylate copolymer may take the form of a random, alternate, block or grafted copolymer.

Mixtures of various acrylate polymers and/or copolymers may be used in the compositions of this invention.

A vinyl aromatic copolymer, or mixture of more than one thereof, may be added as a separate component, or be used as the matrix resin, in the compositions of this invention in addition to, or instead of, being a part of a poly(phenylene ether) blend formed from poly(phenylene ether), polystyrene and/or the above named non-styrenic polymers.

An elastomeric impact modifier may optionally be used in the compositions of this invention. The elastomeric impact modifier suitable for use herein typically has a glass transition temperature ("T<sub>g</sub>") less than 10°C, and preferably less than -5°C, and is effective for the purpose of imparting enough flexibility and freedom of chain rotation to a composition of this invention to improve its toughness; reduce its notch sensitivity; and enable it, in response to the deformation of an applied stress, to recover with stored modulus rather than fracture.

The rubber content of the impact modifier employed in the compositions of this invention can be up to 80 percent, but is preferably greater than 40 percent, and a mixture of two or more elastomeric substances can be used as the impact modifier.

Illustrative examples of elastomeric impact modifiers useful in the compositions of this invention are thermoplastic elastomers, emulsion-type, core-shell graft copolymer elastomers, and olefinic elastomers.

Thermoplastic elastomers are those which are characterized, for example, in that they can be melted and recooled, or dissolved and reformed upon removal of the solvent, without undergoing any significant change in properties. Thermoplastic elastomers are also characterized by the randomness of the shape and size they take on when mixed by shearing forces with the other components making up the compositions of this invention, especially when heat is applied during such mixing. Because thermoplastic elastomer is typically a long chain molecule, segments of a thermoplastic elastomer in the polymer composition matrix are generally elongated, linear ribbons or bands. The molecules tend to fuse and flow together in a continuous structure. However, chain coiling can yield globule-shaped segments of thermoplastic elastomer in the matrix.

The random shape and size assumed in the polymer composition matrix by a thermoplastic elastomer is to be distinguished from the shape and size assumed by a core-shell graft copolymer. A core-shell graft copolymer is typically present in the polymer matrix in a bead shape both before and after mixing by application of shearing forces, whether heat is used or not, and is usually present in a rather narrow size range, for example 0.05-0.8 microns. The retention of this core-shell, or spherical, shape by the graft polymer, even after heating and mixing, results from the fact that the outer layers, which surround the core, are formed by grafting appropriate monomers onto the core. A core-shell graft copolymer typically cannot be melted and recooled without a significant change in properties because the graft polymer will tend to decompose or crosslink, and the bead-shaped segments of graft polymer will tend to agglomerate upon melting, making dispersion of them by mixing difficult.

Thermoplastic elastomers include, for example, an SBR rubber, which is a copolymer of styrene and butadiene typically containing about 23% styrene. The monomers themselves can be randomly dispersed along the backbone, or blocks of each monomer can be randomly dispersed. Thermoplastic elastomers also include the di-block ("A-B") copolymers and the tri-block ("A-B-A") copolymers discussed above with relation to vinyl aromatic copolymers for use in blending with poly(phenylene ether) to form a poly(phenylene ether) blend.

Linear, branched, radial or teleblock A-B-A or A-B block copolymer thermoplastic elastomers can also be prepared from materials other than vinyl aromatic systems. These other copolymers also have a rigid block "A" having a  $T_g$  above room temperature (approximately 23-25°C) and a rubbery block "B" having a  $T_g$  below room

temperature. Examples of typical pairings of the various materials used to form the respective A and B blocks of such other block copolymer thermoplastic elastomers are shown below in Table

Table I  
Block Copolymer Pairings

A block	B block
polyethylene	ethylene/butylene copolymer
polyurethane	polyester polyether
polyester	polyether
polypropylene	EPDM rubber

Block copolymer thermoplastic elastomers can be prepared, for example, by anionic polymerization using an alkyl-lithium initiator. Thermoplastic elastomers based on urethane are discussed in greater detail in Schollenberger, USP 3,015,650 and Saunders, USP 3,214,411; and those based on copolyester-ether are discussed in Witsiepe, USP 3,651,014, each of which is incorporated herein.

Representative examples of the core-shell graft copolymer elastomers suitable for use herein are those which can be based on either a diene rubber, an acrylate rubber or on mixtures thereof.

A diene rubber contains a substrate latex, or core, which is made by polymerizing a diene, preferably a conjugated diene, or by copolymerizing a diene with a mono-olefin or polar vinyl compound, such as styrene, acrylonitrile, or an alkyl ester of an unsaturated carboxylic acid such as methyl methacrylate. The substrate latex is typically made up of about 40-85% diene, preferably a conjugated diene, and about 15-60% of the mono-olefin or polar vinyl compound. The elastomeric core phase should have a glass transition temperature ("T<sub>g</sub>") of less than about 10°C, and preferably less than about -20°C. A mixture of ethylenically unsaturated monomers is then graft polymerized to the substrate latex. A variety of monomers may be used for this grafting purpose, of which the following are exemplary: vinyl compounds such as vinyl toluene or vinyl chloride; vinyl aromatics such as styrene, alpha-methyl styrene or halogenated styrene; acrylonitrile, methacrylonitrile or alpha-halogenated acrylonitrile; a C<sub>1</sub>-C<sub>8</sub> alkyl acrylate such as ethyl acrylate or hexyl acrylate; a C<sub>1</sub>-C<sub>8</sub> alkyl methacrylate such as methyl methacrylate or hexyl methacrylate; glycidyl methacrylate; acrylic or methacrylic acid; and the like or a mixture of two or more thereof.

The grafting monomers may be added to the reaction mixture simultaneously or in sequence, and, when added in sequence, layers, shells or wart-like appendages can be built up around the substrate latex, or core. The monomers can be added in various ratios to each other although, when just two are used, they are frequently utilized in equal amounts. A typical weight ratio for methyl methacrylate/butadiene/styrene copolymer ("MBS" rubber) is about 60-80 parts by weight substrate latex, about 10-20 parts by weight of each of the first and second monomer shells. A preferred formulation for an MBS rubber is one having a core built up from about 71 parts of butadiene, about 3 parts of styrene, about 4 parts of methyl methacrylate and about 1 part of divinyl benzene; a second phase of about 11 parts of styrene; and a shell phase of about 11 parts of methyl methacrylate and about 0.1 part of 1,3-butylene glycol dimethacrylate, where the parts are by weight of the total composition. A diene-based, core-shell graft copolymer elastomer and methods for making same, as described above, are discussed in greater detail in Saito, USP 3,287,443, Curfman, USP 3,657,391, and Fromuth, USP 4,180,494.

An acrylate rubber has a first phase forming an elastomeric core and a second phase forming a rigid thermoplastic phase about said elastomeric core. The elastomeric core is formed by emulsion or suspension polymerization of monomers which consist of at least about 50 weight percent alkyl and/or aralkyl acrylates having up to fifteen carbon atoms, and, although longer chains may be used, the alkyls are preferably  $C_2-C_6$ , most preferably butyl acrylate. The elastomeric core phase should have a  $T_g$  of less than about  $10^\circ C$ , and preferably less than about  $-20^\circ C$ .

The rigid thermoplastic phase of the acrylate rubber is formed on the surface of the elastomeric core using suspension or emulsion polymerization techniques. The monomers necessary to create this phase together with necessary initiators are added directly to the reaction mixture in which the elastomeric core is formed, and polymerization proceeds until the supply of monomers is substantially exhausted. Ethylenically unsaturated monomers such as glycidyl methacrylate, or an alkyl ester of an unsaturated carboxylic acid, for example a  $C_1-C_8$  alkyl acrylate like methyl acrylate, hydroxy ethyl acrylate or hexyl acrylate, or a  $C_1-C_8$  alkyl methacrylate such as methyl methacrylate or hexyl methacrylate, or mixtures of any of the foregoing, are some of the vinyl monomers which can be used for this purpose. Either thermal or redox initiator systems can be used. Because of the presence of the graft linking agents on the surface of the elastomeric core, a portion of the chains which make up the rigid thermoplastic phase are chemically bonded to the elastomeric core. It is preferred that there be at least about 20% bonding of the rigid thermoplastic phase to the elastomeric core.

A preferred acrylate rubber is made up of more than about 40% to about 95% by weight of an elastomeric core and about 60% to about 5% of a rigid thermoplastic phase. The elastomeric core can be polymerized from about 75% to about 99.8% by weight  $C_1-C_6$  acrylate, preferably n-butyl acrylate. The rigid thermoplastic phase can be polymerized from at least

50% by weight of C<sub>1</sub>-C<sub>8</sub> alkyl methacrylate, preferably methyl methacrylate. Acrylate rubbers and methods for making same, as described above, are discussed in greater detail in Owens, USP 3,808,180 and Witman, USP 4,299,928.

Core-shell grafted copolymeric elastomers also include a vinyl nitrile/diene/vinyl aromatic copolymer, as described above with relation to the vinyl aromatic copolymers includable in a poly(phenylene ether) blend, having an elastomeric core which is greater than 40 percent by weight of the copolymer.

Olefinic elastomers useful as an impact modifier in the compositions of this invention are based generally on a long-chain, hydrocarbon backbone, which may or may not be grafted with one or more vinyl monomers. Representative examples of a few olefinic elastomers which illustrate the variation in the known substances which would suffice for such purpose are as follows: butyl rubber; chlorosulfonated polyethylene rubber; ethylene/propylene copolymer and ethylene/propylene/diene copolymer, which may be grafted with one or more vinyl monomers; fluorinated olefins, including polytetrafluoroethylene; neoprene rubber; nitrile rubber; polybutadiene and polyisoprene.

The olefinic elastomer used herein may also contain reactive moieties. A reactive olefinic elastomer may, for example, be a polymer which has a glass transition temperature (T<sub>g</sub>) less than 0°C formed from (I) (A) at least one olefin monomer such as ethylene, propylene, isopropylene, butylene or isobutylene, or at least one conjugated diene such as butadiene, and the like, or mixtures thereof, or (B) a copolymer of one or more olefin monomers, such as described above, with other vinyl monomer(s), but containing a sufficient amount of the olefin monomer(s) to impart a T<sub>g</sub> of less than 0°C to the reactive olefinic elastomer; (II) at least one vinyl (i.e. olefinically unsaturated, including vinylidene) or olefin monomer carrying at least one epoxide group; and, optionally, (III) at least one vinyl (i.e. olefinically unsaturated, including vinylidene) monomer not carrying an epoxide group.

Representative vinyl (i.e. olefinically unsaturated, including vinylidene) monomers useful as the optional component (III) in forming the polymeric reactive olefinic elastomer useful in this invention include the following: vinyl compounds (especially when they bear a polar, electronegative group or functionality) such as vinyl toluene, alphamethyl styrene, halogenated styrene; those containing nitrile groups such as copolymers of acrylonitrile, methacrylonitrile or alpha-halogenated acrylonitrile; a C<sub>1</sub>-C<sub>8</sub> alkyl acrylate or methacrylate such as ethyl acrylate, butyl acrylate, hexyl acrylate, hydroxy ethyl acrylate, methyl methacrylate or hexyl methacrylate; acrylic or methacrylic acid; the vinylidene monomers, especially when they bear a polar, electronegative group or functionality such as a halogen group, or an organic group having a double or triple bond such as phenyl, carboxy, cyano or the like; vinyl esters or vinyl ethers; maleimides; mononitriles having alpha-beta-olefinic unsaturation and lower alkyl or halogen substituents; aliphatic vinyl compounds such as vinyl chloride, vinylidene chloride, amides and nitriles, vinyl acetate, vinyl propionate and

vinyl benzoate; vinyl-methyl-ether, vinyl-ethyl-ether and vinyl-isobutyl-ether; and vinyl aromatic compounds such as styrene, alpha-methyl styrene, vinyl toluene, vinyl xylene, p-ethylstyrene, 2,4-dimethyl styrene, o-chlorostyrene and 2,5-dichlorostyrene; vinyl esters; vinyl ethers; alpha-olefins; the maleates; the fumarates; and the like; or mixtures of two or more of any of the foregoing. In general, vinyl and vinylidene monomers from groups such as the vinyl and vinylidene -esters, -ethers, -organic acids, -aromatics, -alcohols, -anhydrides, -halides, -nitriles and -amides; or mixtures of any of the foregoing may be used. Additionally, any one or more of the foregoing monomers may be copolymerized with carbon monoxide.

Vinyl monomers such as the foregoing may also be copolymerized as part of the olefin copolymer described above as component (I)(B); or, when carrying an epoxide group, may be used as the component (II). Or, the epoxide group may be carried on an olefin monomer.

Suitable olefinically unsaturated monomers containing epoxide groups for use as component (II) of the terpolymeric reactive olefinic elastomer include, for example, glycidyl esters of unsaturated carboxylic acids (glycidyl methacrylate); glycidyl ethers of unsaturated alcohols (allyl-glycidyl-ether) and of alkenylphenols (isopropenylphenyl-glycidylether); and vinyl and allyl esters of epoxycarboxylic acids (vinyl esters of epoxidized oleic acid). In general, all compounds which contain both a polymerizable unsaturated group and reactive epoxide groups in the molecule can be used for preparation of the reactive olefinic elastomer of the invention.

Copolymers of 1-25 percent (by weight) of glycidyl methacrylate, 40-95 percent of ethylene, and 4-40 percent of vinyl acetate are particularly suitable for use herein as the polymeric reactive olefinic elastomer. When the optional component (III) is not present in the reactive olefinic elastomer, a copolymer of 1-25 percent (by weight) of glycidyl methacrylate, 75-99 percent of ethylene is preferred.

Copolymers containing epoxide groups may be obtained according to known processes, for example by radical polymerization in chlorobenzene at 80°C in 50% strength solution. For instance, monomers such as listed above are dissolved in an appropriate solvent, such as benzene, chlorobenzene or toluene, and polymerized at a temperature of about 80°C by adding azobisisobutyronitrile, whereby oxygen is excluded. After the monomers have been reacted, the solvent used is distilled off (e.g., chlorobenzene at 100°C and 20 torr) and the residue is dried in vacuum at 100°C and then powdered. The terpolymeric reactive olefinic elastomer of this invention can also be prepared in gas phase under conditions suitable for polymerizing an olefin. For example, the terpolymer can be made in either a tubular reactor or a stirred autoclave, where heated, pressurized feed streams of olefin or vinyl monomer gas, peroxide free-radical initiator and chain transfer agent are injected into the reaction device.



The reaction of formation usually occurs at 1,500-3,000 atm (152-304 MPa) and at a temperature usually not exceeding 300°C, as known in the art.

The molecular weight of the reactive olefinic elastomer is typically between about 10,000 and about 500,000, preferably between about 30,000 and about 200,000, and it typically contains about 5 to about 1,000, preferably about 20 to about 500, epoxide groups per macromolecule.

Various thermoplastic molding polymers may optionally be included as components in the compositions of this invention. These polymers include polystyrene, polyamide, polyolefin, poly(vinyl chloride), polyurethane, poly(methyl methacrylate) and polyacetal, or a mixture of any of same. Polystyrene, poly(methyl methacrylate) and polyamide have been described above.

A polyolefin may be any of the several different kinds mentioned below including, for example, linear low density polyethylene ("LLDPE"). LLDPE is formed under the kind of low pressure conditions which are usually employed for forming high density polyethylene ("HDPE"). However, a low density product (0.910 - 0.940 g/cm<sup>3</sup>) results because, rather than forming a homopolymer, ethylene is copolymerized with one or more  $\alpha$ -olefins, which in the final product take on the form and function of short side chains. Because the comonomers most frequently used are  $\alpha$ -olefins such as 1-butene, 4-methyl-1-pentene, 1-hexene or 1-octene, these side chains do prevent the close, fully crystalline type of packing representative of HDPE, but they are not nearly as long as the fully branched, long side chains associated with low density polyethylene ("LDPE") made under high pressure conditions.

LLDPE can be formed in a slurry using a light hydrocarbon diluent and a supported chromium catalyst, or it can be formed as a slurry in hexane using organometal-titanium type catalysts. It can also be formed in cyclohexane in solution at a relatively high temperature, approximately 250°C, using as a catalyst a combination of tributyl aluminum, titanium tetrachloride and vanadium oxychloride. LLDPE can also be formed in gas phase using a fluidized bed of growing polymer particles to which a supported chromium oxide catalyst modified with titanium and fluoride is charged, as described in Levine, USP 4,011,382 (incorporated herein), or by a gas-phase process using a stirred but non-fluidized bed and a supported titanium catalyst-triethylaluminum cocatalyst as described in Jezl, USP 4,129,729 (incorporated herein).

LDPE is typically thought of as that which is made under high pressure conditions and has a density between about 0.916 to about 0.930 g/cm<sup>3</sup>. This low density results from the many zones of amorphous arrangement which are characteristic of LDPE because of its long chain branches, which can contain thousands of carbon atoms. LDPE can be made in either a tubular reactor or a stirred autoclave, where heated, pressurized feed streams of ethylene gas, peroxide free-radical initiator and chain transfer agent are injected into the reaction device. The reaction of formation usually occurs at 1,500-3,000 atm (152-304 MPa) and at a

temperature usually not exceeding 300°C, as known in the art. LDPE can be copolymerized with monomers such vinyl acetate, ethyl acrylate, acrylic acid or other polar vinyl monomers.

An HDPE homopolymer is typically about 94% crystalline and has a density of about 0.950 to about 0.970 g/cm<sup>3</sup>. HDPE, because of its much greater crystallinity and density, has a higher melting point than LDPE - 135°C vs. 115°C. The molecular weight of HDPE usually ranges from 50,000 to 1,000,000 or more. One process for making HDPE involves polymerization at about 100-150°C and at about 2-4 MPa (290-580 psi) using a chromium oxide-promoted silica catalyst. HDPE is also manufactured in a slurry system wherein high purity ethylene is fed to a loop reactor which contains a low boiling hydrocarbon used to dissolve the ethylene, and to suspend the catalyst and polymer particles. The temperature is typically between about 70-110°C and the pressure is typically between about 1 and 5 MPa. A chromium catalyst on a powdered silica substrate is typically used. As the polymer particles are formed they are removed from the reactor in a concentrated slurry and are discharged into a flash tank for drying. Alternatively, HDPE can be made in a gas-phase process wherein no hydrocarbon diluent is used and a fluidized bed is used to agitate and suspend the polymer particles. Methods for making HDPE are more particularly described in Hogan, USP 2,825,721 (incorporated herein).

Ziegler process polyethylene ("ZPE") has great versatility because of the wide range of molecular weights in which it can be prepared using the versatile Ziegler catalyst. ZPE can include, for example, waxes ranging in molecular weight from 10,000 to ultrahigh molecular weight HDPE having a molecular weight of several million. ZPE has a density of about 0.940 to about 0.965 g/cm<sup>3</sup>. Both supported and non-supported magnesium-titanium catalyst systems find wide use in the manufacture of ZPE, for example the magnesium dialkyls described in Birkelbach, USP 4,120,820 (Dow). Another group of Ziegler catalysts useful in making polyethylene are those formed by the reaction of organosilols with chromium trioxide, such as described in Baker, USP 3,324,101 (Union Carbide). Ziegler catalysts can be successfully used in suspension, or slurry, systems where the temperature is kept below 110°C and is run at about 0.5 to 2 MPa to avoid solution in the diluent. In solution polymerization, the system is operated at about 150 - 250°C and at about 2 - 4 MPa. Gas-phase polymerization, which is run at 70 - 110°C and at 2 - 3 MPa, does not use a hydrocarbon solvent or diluent.

The preparation of polypropylene also involves the use of Ziegler catalysts, which allows the stereo regular polymerization of propylene to form isotactic polypropylene. The catalyst used is typically a titanium trichloride in combination with aluminum diethylmonochloride, as further described in Cecchin, USP 4,177,160 (incorporated herein). The various types of polymerization processes used for the production of polypropylene include the slurry process, which is run at about 50 - 90°C and 0.5 - 1.5 MPa (5-15 atm), and the gas-phase and liquid-monomer processes, in which extra care must be given to the removal of

amorphous polymer. Functionalized polypropylene, containing functional groups such as maleic anhydride or acrylic acid, is also suitable for use herein.

Various higher olefins can be homopolymerized to form polyolefins using Ziegler-Natta catalysts, among them 1-butene and 4-methyl-1-pentene. 1-Butene is polymerized in  
5 solution using an aluminum-reduced  $TiCl_3$  catalyst with diethylaluminum chloride as the cocatalyst, as described in Edwards, USP 3,362,940 (incorporated herein). 4-Methyl-1-pentene is prepared by the dimerization of propylene in slurry at about 180°C and 6-7 MPa, as further described in Hashimoto, USP 3,950,450 (incorporated herein).

Poly(vinyl chloride) is prepared, for example, by mass or suspension  
10 polymerization. In suspension polymerization, liquid monomer is dispersed under pressure in an aqueous solution containing a protective colloid and a monomer-soluble free radical initiator, such as a diacetyl peroxide or an alkyl peroxyester. Polymerization ensues when the reaction mixture is heated to 50-75°C. Other vinyl monomers can also be copolymerized along with the vinyl chloride monomer.

15 A polyurethane is typically prepared from a formulation of a polyisocyanate or diisocyanate "A" component, and an active-hydrogen-containing "B" component such as a polyol, polythiol or a polyamine or a combination thereof.

Polyurethane components which are preferred include those containing methylene diphenyldiisocyanate (MDI), polymeric MDI (PMDI), MDI prepolymers, and modified  
20 MDI. However, any kind of di- or polyisocyanate can be used to prepare a polyurethane for use in the present invention. These materials include but are not limited to aliphatic, cycloaliphatic and preferably multivalent isocyanates such as 1,6-hexamethylenediisocyanate; 1-isocyanato-3,5,5-trimethyl-1-3-isocyanatomethyl-cyclohexane; 2,4- and 2,6-hexahydrotoluenediisocyanate, as well as the corresponding isomeric mixtures; 4,4', 2,2'- and  
25 2,4'-dicyclohexylmethanediisocyanate, as well as the corresponding isomeric mixtures; 2,4- and 2,6-toluenediisocyanate and the corresponding isomeric mixtures.

As stated hereinabove MDI based materials are preferred. These materials include 4,4', 2,4'- and 2,2'-diphenylmethanediisocyanate and the corresponding isomeric mixtures; mixtures of 4,4', 2,4'- and 2,2'-diphenylmethanediisocyanates and PMDI; and  
30 mixtures of PMDI and toluene diisocyanates. Mixtures of MDI and MDI based materials with any other isocyanate group containing material can be used in the present invention.

Also advantageously used for the isocyanate starting materials in polyurethane preparation are the so-called modified multivalent isocyanates, i.e., products which are obtained through chemical reactions of the above diisocyanates and/or polyisocyanates.  
35 Exemplary are polyisocyanates containing esters, ureas, biurets, allophanates and preferably carbodiimides; isocyanurate and/or urethane group containing diisocyanates; and/or polyisocyanates. Individual examples are aromatic polyisocyanates containing urethane groups, preferably having isocyanate group contents of from about 2 to about 40 weight

percent, more preferably about 20 to 35 weight percent, obtained by reaction of diisocyanates and/or polyisocyanates with, for example, lower molecular weight diols, triols, oxyalkylene glycols, dioxyalkylene glycols or polyoxyalkylene glycols having molecular weights up to about 800. These polyols can be employed individually or in mixtures as di- and/or polyoxyalkylene glycols. For example, diethylene glycols, dipropylene glycols, polyoxyethylene glycols, polyoxypropylene glycols and polyoxypropylenepolyoxyethylene glycols can be used.

Suitable also are prepolymers containing isocyanate (NCO) groups, having NCO contents of from 2 to 30 weight percent, more preferably from 15 to 25 weight percent. Liquid polyisocyanates containing carbodiimide groups and/or isocyanurate rings, having NCO contents of from 8 to 40 weight percent, more preferably from 20 to 35 weight percent, can also be used.

The active hydrogen containing compounds useful for preparing a polyurethane are generally known and are described in such publications as High Polymers, Vol. XVI, "Polyurethanes, Chemistry and Technology" by Saunders and Frisch, Interscience Publishers, New York, Vol. I, pp. 32-42, 44-54 (1962) and Vol. II, pp. 5-6, 198-199 (1964); Organic Polymer Chemistry by K. J. Saunders, Chapman and Hall, London, pp. 323-325 (1973); and Developments in Polyurethanes, Vol. I, J. M. Burst, ed., Applied Science Publishers, pp. 1-76 (1978). Preferred are compounds such as dipropylene glycol, ethylene glycol, diethyltoluenediamine polyol, polyether diols and triols, polyester diols and triols, mixtures of the above and the like. However, any active hydrogen containing compound can be used with the method of this invention. Examples of such materials include those selected from the following classes of compositions, alone or in admixture: (a) alkylene oxide adducts of polyhydroxyalkanes; (b) alkylene oxide adducts of non-reducing sugars and sugar derivatives; (c) alkylene oxide adducts of phosphorus and polyphosphorus acids; and (d) alkylene oxide adducts of polyphenols. Polyols of these types are referred to herein as "base polyols". Examples of alkylene oxide adducts of polyhydroxyalkanes useful herein are adducts of ethylene glycol, propylene glycol, 1,3-dihydroxypropane, 1,4-dihydroxybutane, and 1,6-dihydroxyhexane, glycerol, 1,2,4-trihydroxybutane, 1,2,6-trihydroxyhexane, 1,1,1-trimethylolethane, 1,1,1-trimethylolpropane, pentaerythritol, polycaprolactone, xylitol, arabitol, sorbitol, mannitol, and the like. Preferred herein as alkylene oxide adducts of polyhydroxyalkanes are the ethylene oxide adducts of trihydroxyalkanes. Other useful adducts include ethylene diamine, glycerin, ammonia, 1,2,3,4-tetrahydroxy butane, fructose, and sucrose.

Also preferred are poly(oxypropylene) glycols, poly(oxybutylene) glycols, triols, tetrols and hexols and any of these that are capped with ethylene oxide. These polyols also include poly(oxypropylene-oxyethylene)polyols. The oxyethylene content should preferably comprise less than about 80 weight percent of the total and more preferably less than about 40 weight percent. The ethylene oxide, when used, can be incorporated in any way along the polymer

chain, for example, as internal blocks, terminal blocks, or randomly distributed blocks, or any combination thereof.

The base polyols described hereinabove can contain small amounts of "inherent" unsaturation, i.e., unsaturation due to the isomerization of propylene oxide to allyl alcohol during the manufacture of the polyol. In some cases it may be desirable to include additional unsaturation in the polyols for graftin purposes.

Polymercaptans and other isocyanate-reactive compounds are also suitable in the present invention. Polyisocyanate polyaddition active hydrogen containing compounds (PIPA) are particularly preferred for use with the present invention. PIPA compounds are typically the reaction products of TDI and triethanolamine. A method for preparing PIPA compounds can be found in, for example, United States Patent 4,374,209, issued to Rowlands.

Another preferred class of polyols are "copolymer polyols", which are base polyols containing stably dispersed polymers such as acrylonitrile-styrene copolymers. Production of these copolymer polyols can be from reaction mixtures comprising a variety of other materials, including, for example, catalysts such as azobisisobutyronitrile; copolymer polyol stabilizers; and chain transfer agents such as isopropanol. Polyurethane formulations containing the above compounds are commonly commercially available.

A polyacetal is a polymer which arises by the bond opening and polymerization of the carbonyl group of an aldehyde.

A variety of flame or ignition resistance additives may be advantageously include in the compositions of this invention. Representative examples thereof include antimony oxides; sodium antimonate; metal borates (particularly zinc); boric acid; alumina trihydrate; ammonium fluoroborate; molybdenum oxide; halogenated hydrocarbons; 5 decabromomdiphenyl oxide; 1,2-bis(2,4,6-tribromophenoxy) ethane; halogenated carbonate oligomers; halogenated diglycidyl ethers; tetrabromo phthalic anhydride; inorganic phosphorous compounds such as ammonium phosphates; organophosphorous compounds such as alkyl acid phosphates, trialkyl phosphates (such as triethyl), dimethyl methyl phosphonate, halogenated alkyl phosphates and phosphonates such as 1,3-dichloro-2- 10 propanol phosphate, diphosphates, 3,9-tribromoneopentoxy-2,4,8,10-tetraoxa-3,9-diphosphaspiro(5.5)undecane-3,9-dioxide, oligomeric cyclic and phenyl phosphonates (including halogenated), trisaryl phosphates (including halogenated), phosphine oxides; poly(tetrafluoroethylene); and metal salts of aromatic sulfur compounds such as sulfates, bisulfates, sulfonates, sulfonamides and sulfimides; and others as set forth in Laughner, U.S. 15 Pat. No. 4,786,686, which is incorporated herein.

A variety of other additives may be used in the compositions of this invention for protection against thermal, oxidative and ultra-violet degradation. Representative of the thermal and oxidative stabilizers which can be advantageously utilized are hindered phenols, hydroquinones, phosphites, including substituted members of those groups and/or mixtures of 20 more than one thereof. A preferred phenolic anti-oxidant is Irganox™ 1076 anti-oxidant, available from Ciba-Geigy Corp. Ultra-violet stabilizers such as various substituted resorcinols, salicylates, benzotriazoles, benzophines, hindered amines and hindered phenols can also be usefully included in the compositions hereof, as can be lubricants, colorants, fillers such as talc, clay, phosphate, metal, inorganic or graphite fibers, or mica, dyes, pigments, mold release 25 agents, and reinforcement agents such as fiberglass or phosphate, metal, inorganic or graphite fibers. Additives and stabilizers of the same or a similar kind as the foregoing are known, and the use and selection thereof is within the skill in the art. However, such additives, if used, typically do not exceed 15 percent by weight of the total composition, except fillers or reinforcing agents, which may constitute up to 40 percent of the composition.

30 Examples of several preferred embodiments of the compositions of this invention wherein polycarbonate and polyester constitute the matrix resin are set forth below. It is not intended, however, that these examples (Examples 1a to 26a) should in any manner restrict the scope of this invention. Some of the particularly desirable features of this invention may be seen by contrasting the characteristics of Examples 1a to 26a with those of various controlled 35 formulations (Controls Aa to La) which do not possess the features of, and are not therefore embodiments of, this invention.

The polycarbonate/polyester compositions prepared in Controls Aa to La and Examples 1a to 26a are made by dry blending the ingredients thereof and agitating same in a

paint shaker for 7 minutes. The dry blended formulations are then melt mixed in a vented 30mm Werner-Pfleiderer co-rotating, twin screw extruder using a 240 rpm speed and a set temperature of 290°C. Each extruded composition is passed through a water bath, chopped into granules and collected for molding. Granules are thoroughly dried in a circulated air oven at 120°C for 4 to 6 hours prior to molding. All testing samples are prepared by injection molding on a 75 ton (6.8 x 10<sup>4</sup> kg) Arburg molding machine. Molding temperatures for the barrel and mold are set at 290°C and 175°F, respectively. Testing samples for gloss measurement are molded in the form of a 2.5 in x 6.5 in plaque, while physica properties were determined from samples molded on an ASTM mold set at 175°F.

The formulations of the polycarbonate/polyester compositions of Controls Aa to La and Examples 1a to 26a are given below in Tables IIa to IXa in parts by weight of the total composition. In Tables IIa to IXa:

"PC" is a polycarbonate having a melt flow rate of 13, as determined according to ASTM Designation D 1238-89, Condition 300/1.2, available from The Dow Chemical Company;

"PET I" is Tratuf™ 9506 poly(ethylene terephthalate) having an 0.95 intrinsic viscosity, available from Goodyear Tire and Rubber Company;

"PET II" is poly(ethylene terephthalate) having an 0.72 intrinsic viscosity, available from Eastman Kodak;

"PPE I" is Noryl™ N-300 poly(phenylene ether)/styrenic polymer alloy having a heat deflection temperature under load of 300°F, available from General Electric Company;

"PPE II" is Noryl™ N-225 poly(phenylene ether)/styrenic polymer alloy having a heat deflection temperature under load of 225°F, available from General Electric Company;

"PPE III" is Noryl™ N-190 poly(phenylene ether)/styrenic polymer alloy having a heat deflection temperature under load of 190°F, available from General Electric Company;

"PPE IV" is unalloyed poly(phenylene ether), available from Aldrich;

"PPE/PMMA blend" is a 50/50 weight ratio blend of poly(phenylene ether) and poly(methyl methacrylate), prepared by melt mixing a dry mix of the two polymers at 300°C, the poly(methyl methacrylate) having a heat deflection temperature under load at 264 psi of 199°F, determined according to ASTM Designation D648-82, and being available from Rohm & Haas Company;

"PPE/PET blend" is a 50/50 weight ratio blend of poly(phenylene ether) and PET I, prepared by melt mixing a dry mix of the two polymers at 300°C;

"Elvax™ 3152" copolymer is ethylene/vinyl acetate copolymer available from E.I. du Pont de Nemours & Co.;

"Paraloid™ 3339" elastomeric copolymer is a butylate acrylate core-shell elastomer, available from Rohm & Haas Company;

"Paraloid™ 8967" elastomeric copolymer is a methacrylate/butadiene/styrene core-shell elastomer, available from Rohm & Haas Company;

"GRC 120" is acrylonitrile/butadiene/styrene core shell impact modifier, available from The Dow Chemical Company;

"Kraton™ G 1750" copolymer is a hydrogenated styrene/butadiene radial block thermoplastic elastomeric copolymer, available from Shell Oil Company;

5 "Kraton™ G 1702" copolymer is a hydrogenated styrene/butadiene di-block thermoplastic elastomeric copolymer, available from Shell Oil Company;

"Kraton™ G 1651" copolymer is a hydrogenated styrene/butadiene/styrene tri-block thermoplastic elastomeric copolymer, available from Shell Oil Company;

10 "ABS 19" is mass produced acrylonitrile/butadiene/styrene copolymer having approximately 20 percent rubber, available from The Dow Chemical Company;

"Reactive PS" is a polystyrene which incorporates 1 weight percent  $C_3NOH_4$  oxazoline ring onto the polystyrene backbone, available from The Dow Chemical Company;

"Vistalon™ 3708" copolymer is an ethylene/propylene/diene monomer thermoplastic elastomer, available from Exxon Corp.;

15 "Carbon black" is powdered black pigment;

"IR 1076" is phenolic anti-oxidant stabilizer, available from Ciba-Geigy Corporation;

"BC-52" is Tetrabromo Bisphenol-A carbonate oligomer, available from Great Lakes Chemical, Inc.;

20 "TPP" is triphenyl phosphate, available from Akzo Chemicals, Inc.; and

"Teflon™ 6C" polymer is a fibril form of poly(tetrafluoroethylene), available from E.I. duPont de Nemours & Co.

In Control La and Example 26a, polycarbonate, polyester and Kraton™ G 1651 copolymer were pre-extruded and added to the poly(phenylene ether) alloy (PPE III) at the  
25 molding machine as a salt-and-pepper blend.

Gloss measurements are performed on testing samples according to ASTM Designation D 523-85 using a Dr. Lange Reflectometer RB3 available from Hunter Associates.

Impact resistance is measured by the Izod test according to ASTM Designation D 256-84 (Method A) at 23°C. The notch is 10 mils (0.254 mm) in radius. In "PR Izod", the notch is  
30 cut so that the flexural shock caused by the striking nose of the pendulum is propagated parallel to the direction of flow taken by the molten extrudate during formation of the sample. In "PL Izod", the notch is cut so that the flexural shock caused by the striking nose of the pendulum is propagated perpendicular to the direction of flow taken by the molten extrudate during formation of the sample. Weldline impact resistance ("Weldline Izod") is also measured  
35 by the Izod test according to ASTM Designation D 256-84 (Method A) at 23°C, but with respect to a sample which is formed with a butt weld in a double gated mold. The sample is unnotched, and it is placed in the vise so that the weld is coincident with the top surface of the vise jaws. All Izod results are reported in ft-lb/in.



The U.L. 94 burn test is performed on the samples molded from the compositions of Control E and Examples 9-11.

The results of the various measurements are also reported in Tables IIa to IXa.

In Tables IIa to IXa, Controls Aa to La are indicated by C-Aa, C-Ba, C-Ca etc., and

5 Examples 1a to 26a are indicated by E-1a, E-2a, E-3a etc.

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Table IIa

	C-Aa	C-Ba	C-Ca	C-Da	E-1a	E-2a	E-3a	E-4a	E-5a
PC	1,500	1,225	1,225	1,225	1,500	1,125	1,125	1,125	1,125
PET I	500	600	600	600	400	600	600	600	600
Elvax™ 3152		175				175			
Paraloid™ 3339			175				175		
Paraloid™ 8967				175				175	
GRC 120									175
PPE I					100	100	100	100	100
20° Gloss	90	85	88	73	19	5	16	24	9
Weldline Izod		0.8	13.3	15.0	10.0	1.5	19.1	17.4	8.7

Table IIIa

	E-6a	E-7a	E-8a	C-Ea	E-9a	E-10a	E-11a
PC	1,276	1,316	1,376	1,090	1,040	1,020	1,000
PETI	500	460	360	600	600	600	600
Kraton™ G-1651	140	140	140	100	100	100	100
Reactive PS			40				
PPEI					50	50	50
PPE/PMMA blend	80						
PPE/PET blend		80	80				
Carbon black	4	4	4				
BC-52				200	200	60	
Teflon™ 6C				10	10	10	10
TPP						60	140
20° Gloss	19	12	20	77	17	16	48
60° Gloss	70	62	75	98	70	69	89
U.L., 94, 1/8"				V-0	V-0	V-0	V-0

Table IVa

	C-11a	C-12a	C-13a	C-14a	C-15a	C-16a	C-17a
PC	1,460	1,220	1,000	750	1,420	1,160	920
PET II	400	600	800	1,000	400	600	800
Kralon™ G 1651	140	180	200	250	140	180	200
PPE I					40	60	80
PPE II							
IR 1076	4	4	4	4	4	4	4

Table Va

	C-Fa	C-Ga	C-Ha	C-Ia	E-12a	E-13a	E-14a	E-15a	E-16a
20° Gloss	80	73	67	71	10	21	25	30	8
Weldline Izod	20.3	7.0	7.3	5.7	23.4	15.2	17.4	25.9	
PR Izod, 23°C	11.7	11.7	11.9	4.0	12.3	12.9	12.7	4.2	13.7
PR Izod, 0°C	8.7	6.4	3.9		11.6	11.6	4.3		14.1
PR Izod, -20°C	4.0	3.1			6.2	4.3			3.7
PL Izod, 23°C	14.0	11.4	11.7	8.7	14.6	14.6	16.9	12.2	13.6
PL Izod, 0°C	13.0	4.4	4.8	3.2	14.1	13.7	4.6	4.0	
PL Izod, -20°C	4.7				6.9	4.9			4.6

Table VIa

	C-Ja	E-17a	E-18a	E-19a	E-20a	E-21a	E-22a	E-23a
PC	1,460	1,450	1,440	1,400	1,300	1,300	1,300	1,100
PET I	400	400	400	400	500	500	600	600
Kraton™ G 1760					150			
Kraton™ G 1702						150		
Kraton™ G 1651	140	140	140	140			100	100
ABS 941							150	
Vistalon™ 3708								100
PPE I		10	20	60	50	50	50	100

Table VIIa

	C-Ja	E-17a	E-18a	E-19a	E-20a	E-21a	E-22a	E-23a
20° Gloss	79	43	35	18	29	9	22	13
Weldline Izod	3.3	3.2	13.8	21.7	1.4	8.0	4.9	5.3
PR Izod, 23°C	11.5	12.2	12.9	12.4	10.2	12.4	11.5	12.6
PR Izod, 0°C		11.7	12.0	11.8	7.8	11.7	8.3	
PL Izod, 23°C	13.1	14.0	14.0	13.9	13.3	12.7	12.7	10.9
PL Izod, 0°C	11.2	11.0	12.8	13.7	8.3	10.3		

Table VIIIa

	C-Ka	E-24a	E-25a	C-La	E-26a
PC	1,460	1,450	1,440	1,400	1,650
PET I	400	400	400	400	200
PPE III					50
PPE IV		10	20		
Kraton™ G 1651	140	140	140	200	100



Table IXa

	C-Ka	E-24a	E-25a	C-La	E-26a
20° Gloss	79	48	33	78	43
60° Gloss				97	88
Weldline Izod	3.3	19.9	24.9		
PR Izod, 23°C	11.5	12.0	12.7		
PR Izod, 0°C		11.7	12.1		
PL Izod, 23°C	13.1	14.2	14.9		
PL Izod, 0°C	11.2	13.0	15.0		
PL Izod, -20°C	3.7	5.1	8.2		

The results of the tests performed on the plaques molded from the compositions of Controls Aa to La and Examples 1a to 26a demonstrate the lower level of gloss, particularly at 20°, which characterizes the plaques molded from the compositions containing poly(phenylene ether). Small quantities of poly(phenylene ether), 5 weight percent of the composition or less (for example 4.5 weight percent or less, or 3 weight percent or less), are typically sufficient to achieve this effect. The presence of poly(phenylene ether) does not detract from the effect of ignition resistance additives in the blend, as shown by Example 9a. The samples molded from Examples 1a to 26a also showed uniform color with reduced pearlescence, high weldline strength and were characterized by reduced delamination effects.

10 The composition of Example 1a had reduced die swell which indicates fine dispersion of the two phases and results in enhanced processibility.

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	C-Ab	E-1b	E-2b	E-3b	E-4b	E-5b	E-6b	E-7b	E-8b
PC I	1,300	1,290	1,270	1,260	1,240	1,260	1,260	1,260	1,270
ABS 29							660		
ABS 55	700	690	670	660	640	660			
ABS 73								660	670
Kraton™ G 1651				40	60	60	60	60	40
PPE I		20	60	40	60	20	20	20	20
20° Gloss	71	62	42	38	22	48	46	16	17
60° Gloss	99	95	86	82	72	87	86	66	68

	C-Bb	E-9b	C-Cb	E-10b	C-Db	E-11b	C-Eb	E-12b
PC II	1,500	1,420	1,400	1,320	1,500	1,420	1,400	1,320
ABS 19					500	500	500	500
ABS 32	500	500	500	500				
Kraton™ G-1851			100	100			100	100
PPE I		80		80		80		80
20° Gloss	69	19	47	7	44	18	51	8
60° Gloss	96	69	81	44	91	69	87	49

	C-Fb	C-Gb	E-13b	E-14b	E-15b	E-16b	E-17b	E-18b	E-19b
PC I		1,300	1,260	1,260	1,270	1,270	1,260	600	1,220
ABS 73					660	670	660	1,200	600
ASA		700	660	660					
Kraton™ D 1102			60		60				
Kraton™ Q 1651	200			60		40	60	160	120
PPE I	1,800					20	20		
PPE II									60
PPE III			20	20	10			40	
20° Gloss	90	100	61	61	11	17	16	4	10
60° Gloss	99	107	91	90	58	68	66	32	55

	C-Hb	E-20b	E-21b	C-Ib	E-22b	E-23b	E-24b	E-25b	E-26b
PCII	1,600	1,600	1,220	1,400	1,300	1,240	1,260	1,270	595
SAN	400	400							
ABS29			600	600	600	600	660	660	1,200
Kraton™ D 1102		80						60	
Kraton™ G 1651			120			60	60		160
PPE I					100	80	20		
PPE II			60						
PPE III		20						10	5
20° Gloss	102	14	26	77	23	13	46	13	42
60° Gloss	105	68	73	99	72	63	86	64	83

	C-Jb	E-27b	E-28b	C-Kb	E-29b	E-30b
PC II	1,400	1,300	1,240	1,800	1,720	1,400
ABS 29	600	600	600			
Polystyrene						400
Kraton™ G 1651			60	200	200	100
PPE 1		100	80		80	100
Carbon Black	4	2	2	4	3	3
20° Gloss	77	23	13	57	8	29
60° Gloss	99	72	63	91	50	82
Weldline Izod	1.76	1.78	2.04	3.5	24.0	

	C-Lb	E-31b	C-Mb	E-32b	E-33b
5 PCI			1,730	1,660	1,660
PC III	1,340	1,275			
ABS 32	335	320			
ABS 61			50	48	48
MBS	80	80	60	58	58
10 Kraton™ G 1651					40
PPE I		80		80	40
BC-52	100	100			
TPP	120	120	150	144	144
Teflon 6C	15	15	10	10	10
15 IR 1076	4	4			
Tinuvin 329	6	6			
20° Gloss	43	16	44	15	20
60° Gloss	90	66	91	63	71
20 U.L. 94, 1/8"	5V	5V	5V	5V	5V
D.T.U.L., °F	217	217	218	253	256

	C-Nb	C-Ob	E-34b	E-35b	E-36b
2 PCI	1,320	1,250	1,210	1,210	1,200
ABS 39	680	650	650	630	600
Bondfast™ 2B		100	100	20	60
3 Vextra™ DPX-518				100	100
Noryl™ N-300			40	40	40
IR 1076	4	4	4	4	4
20° Gloss	67	44	31	10	16
3 60° Gloss	91	94	86	58	71



Examples of several preferred embodiments wherein a vinyl aromatic copolymer is the matrix resin in the compositions of this invention are set forth below. It is not intended, however, that these examples (Examples 1c to 27c) should in any manner restrict the scope of this invention. Some of the particularly desirable features of this invention may be seen by contrasting the characteristics of Examples 1c to 27c with those of various controlled formulations (Controls Ac to Kc) which do not possess the features of, and are not therefore embodiments of, this invention.

The vinyl aromatic copolymer compositions prepared in Controls Ac to Kc and Examples 1c to 27c are made by dry blending the ingredients thereof and agitating same in a paint shaker for 7 minutes. The dry blended formulations are then melt mixed in a vented 30mm Werner-Pfleiderer co-rotating, twin screw extruder using a 250 rpm speed and a set temperature of 240-280°C. Each extruded composition is passed through a water bath, chopped into granules and collected for molding. Granules are thoroughly dried in a circulated air oven at 85°C for 4 to 6 hours prior to molding. All testing samples are prepared by injection molding on a 75 ton (6.8 x 10<sup>4</sup> kg) Arburg molding machine. Molding temperatures for the barrel and mold are set at 240-260°C and 130-150°F, respectively. Testing samples for gloss measurement are molded in the form of a 2.5 in x 6.5 in plaque.

The formulations of the styrenic copolymer compositions of Controls Ac to Kc and Examples 1c to 27c are given below in Tables IIc to VIc in parts by weight of the total composition. In Tables IIc to VIc:

"PC" is a polycarbonate having a melt flow rate of 10, as determined according to ASTM Designation D 1238-89, Condition 300/1.2 (molecular weight of approximately 28,000), available from The Dow Chemical Company;

"PPE I" is Noryl™ N-300 poly(phenylene ether)/styrenic polymer alloy having a heat deflection temperature under load of 300°F, available from General Electric Company;

"PPE II" is Noryl™ N-225 poly(phenylene ether)/styrenic polymer alloy having a heat deflection temperature under load of 225°F, available from General Electric Company;

"PPE III" is Noryl™ N-190 poly(phenylene ether)/styrenic polymer alloy having a heat deflection temperature under load of 190°F, available from General Electric Company;

"PPE IV" is Noryl™ GTX 910 poly(phenylene ether)/nylon/styrenic polymer alloy, available from General Electric Company;

"PPE V" is unalloyed poly(phenylene ether) available from Aldrich;

"PPE/PMMA blend" is a 50/50 weight ratio blend of poly(phenylene ether) and poly(methyl methacrylate), prepared by melt mixing a dry mix of the two polymers at 300°C;

"PPE/ABS blend" is a 50/50 weight ratio blend of poly(phenylene ether) and acrylonitrile/butadiene/styrene copolymer, prepared by melt mixing a dry mix of the two polymers at 300°C;

"Kraton™ G 1651" copolymer is a hydrogenated styrene/butadiene/styrene tri-block thermoplastic elastomeric copolymer, available from Shell Oil Company;

5 "ABS 29" is emulsion produced acrylonitrile/butadiene/styrene copolymer having approximately 20 weight percent rubber, available from The Dow Chemical Company;

"ABS 32" is mass produced acrylonitrile/butadiene/styrene copolymer having approximately 7 weight percent rubber, available from The Dow Chemical Company;

"ABS 39" is emulsion produced acrylonitrile/butadiene/styrene copolymer having approximately 24 weight percent rubber, available from The Dow Chemical Company;

10 "ABS 73" is a blended mass/emulsion produced hybrid acrylonitrile/butadiene/styrene/phenyl maleimide copolymer having approximately 16 weight percent rubber, available from The Dow Chemical Company;

"Polystyrene" is polystyrene, available from The Dow Chemical Company;

15 "SAN" is styrene/acrylonitrile copolymer, available from The Dow Chemical Company;

"PMMA" is Plexiglas™ V-052 poly(methyl methacrylate) having a heat deflection temperature under load at 264 psi of 199°F (determined according to ASTM Designation D648-82), available from Rohm & Haas Company;

"Nylon 6/6" is polyamide, available from E.I. du Pont de Nemours & Co.;

20 "Carbon black" is powdered black pigment; and

"PET" is Tratuf™ 9506 poly(ethylene terephthalate) having an 0.95 intrinsic viscosity, available from Goodyear Tire and Rubber Company.

Gloss measurements are performed on testing samples according to ASTM Designation D 523-85 using a Dr. Lange Reflectometer RB3 available from Hunter Associates.

25 Results of gloss measurements are also reported in Tables IIc to VIc.

In Tables IIc to VIc, Controls Ac to Kc are indicated by C-Ac, C-Bc, C-Cc etc., and Examples 1c to 27c are indicated by E-1c, E-2c, E-3c etc.

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Table IIc

	C-Ac	C-Bc	E-1c	E-2c	E-3c	E-4c	E-5c
SAN	2,000	1,850	1,900	1,800	1,700	1,900	1,800
Kraton™ Q 1651				100	200		100
Polystyrene		150					
PPE II						100	100
PPE III			100	100	100		
Carbon black	4	4	2	4	3	4	4
20° Gloss	92	93	8	6	2	15	6
60° Gloss	100	100	43	37	19	54	37

Table IIIc

	C-Cc	C-Dc	E-6c	E-7c	E-8c	E-9c	C-Ec	E-10c	E-11c	E-12c	E-13c
ABS 29	2,000	1,900	1,900	1,900	1,900	1,900	1,800	1,800	1,800	1,800	1,800
Kraton™ G-1651							100	100	100	100	100
Polystyrene		100					100				
PPE I					100					100	
PPE II				100					100		
PPE III			100					100			
PPE V						100					100
Carbon Black	4	4	4	4	4	4	4	4	4	4	4
20° Gloss	85	83	88	36	24	31	71	37	26	28	25
60° Gloss	97	96	94	79	68	70	91	82	74	72	67

Table IVc

	C-Fc	E-14c	E-15c	C-Gc	E-16c
ABS 32	2,000	1,900	1,800		
ABS 73				2,000	1,800
Kraton™ G 1651			100		100
PPE I		100	100		
PPE II					100
Carbon Black	4	2	3	4	4
20° Gloss	25	19	15	85	4
60° Gloss	72	69	62	96	30

Table Vc

	C-Hc	C-Ic	C-Jc	C-Kc	E-17c	E-18c	E-19c	E-20c	E-21c
SAN	2,000	1,850			1,900	1,800	1,700	1,900	1,800
Kraton™ G 1651				200		100	200		100
Polystyrene		150	1,900						
PPE I				1,800					
PPE II								100	100
PPE III			100		100	100	100		
20° Gloss	92	93	97	90	8	6	2	15	6
60° Gloss	100	100	103	99	43	37	19	54	37

Table VIc

	E-22c	E-23c	E-24c	E-25c	E-26c	E-27c
ABS 29	1,900	1,900				
ABS 39			950	900		875
ABS 73					900	
Kraton™ Q 1661				100	100	100
Nylon 6/6			950	900	900	
PET						925
PPE III	100	100				
PPE IV					100	
PPE/ABS blend			100	100		100
20° Gloss	68	65	68	35	15	18
60° Gloss	94	91	92	78	62	65

The results of the tests performed on the plaques molded from the compositions of Controls Ac to Kc and Examples 1c to 23c demonstrate the lower level of gloss, particularly at 20°, which characterizes the plaques molded from the compositions containing poly(phenylene ether). Examples 24c to 27c demonstrate lower gloss levels of compositions containing blends of styrenic copolymers with other thermoplastic resins and low levels of poly(phenylene ether). Small quantities of poly(phenylene ether), 5 weight percent of the composition or less (for example 4.5 weight percent or less, or 3 weight percent or less), are typically sufficient to achieve this effect. The presence of poly(phenylene ether) does not detract from the effect of ignition resistance additives in the blend. The samples molded from Examples 1c to 27c showed uniform color with reduced pearlescence and were characterized by reduced gloss.

Examples of several preferred embodiments wherein an acrylate polymer or copolymer is the matrix resin in the compositions of this invention are set forth below. It is not intended, however, that these examples (Examples 1d to 10d) should in any manner restrict the scope of this invention. Some of the particularly desirable features of this invention may be seen by contrasting the characteristics of Examples 1d to 10d with those of various controlled formulations (Controls Ad to Cd) which do not possess the features of, and are not therefore embodiments of, this invention.

The acrylate compositions prepared in Controls Ad to Cd and Examples 1d to 10d are made by dry blending the ingredients thereof and agitating same in a paint shaker for 7 minutes. The dry blended formulations are then melt mixed in a vented 30mm Werner-Pfleiderer co-rotating, twin screw extruder using a 250 rpm speed and a set temperature in the range of 240°C-280°C, the set temperature being sufficient in relation to the  $T_g$  of the material to obtain melting thereof in the extruder. Each extruded composition is passed through a water bath, chopped into granules and collected for molding. Granules are thoroughly dried in a circulated air oven at 100°C for 4 to 6 hours prior to molding. All testing samples are prepared by injection molding on a 75 ton (6.8 x 10<sup>4</sup> kg) Arburg molding machine. Molding temperatures for the barrel and mold are set at 250°C-280°C and 150°F, respectively. Testing samples are molded in the form of a 2.5 in x 6.5 in plaque.

The formulations of the acrylate compositions of Controls Ad to Cd and Examples 1d to 6d are given below in Table II d in parts by weight of the total composition. In Table II d:

"(1) PMMA" is Plexiglas™ V-052 poly(methyl methacrylate) having a heat deflection temperature under load at 264 psi of 199°F (determined according to ASTM Designation D648-82), available from Rohm & Haas Company;

"(2) ABS" is emulsion produced acrylonitrile/butadiene/styrene copolymer having approximately 24 percent rubber, available from The Dow Chemical Company;

"(3) PC I" is a polycarbonate having a melt flow rate of 10, as determined according to ASTM Designation D 1238-89, Condition 300/1.2 (molecular weight of approximately 28,000), available from The Dow Chemical Company;



"(4) Kraton™ G 1651" is a hydrogenated styrene/butadiene block thermoplastic elastomeric copolymer, available from Shell Oil Company;

"(5) PPE I" is Noryl™ N-300 poly(phenylene ether)/styrenic polymer alloy having a heat deflection temperature under load of 300°F, available from General Electric Company;

5       "(6) PPE/PMMA blend" is a 50/50 weight ratio blend of poly(phenylene ether) and the poly(methyl methacrylate) used as component 1, prepared by melt mixing a dry mix of the two polymers at 300°C;

10       "(7) PPE/ABS blend" is a 50/50 weight ratio blend of poly(phenylene ether) and the acrylonitrile/butadiene/styrene copolymer used as component 2, prepared by melt mixing a dry mix of the two polymers at 300°C; and

      "(8) Carbon black" is powdered black pigment.

15       In Table IId, Controls Ad to Cd are indicated by C-Ad, C-Bd and C-Cd, and Examples 1d to 6d are indicated by E-1d through E-6d. Gloss measurements are performed on the testing samples molded from the compositions of Controls Ad to Cd and Examples 1d to 6d according to ASTM Designation D 523-85 using a Dr. Lange Reflectometer RB3 available from Hunter Assocaiates. The results of those measurements are also reported in Table IId.

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Table IIId

	C-Ad	E-1d	E-2d	C-Bd	E-3d	E-4d	C-Cd	E-5d	E-6d
(1) PMMA	2,000	1,900	1,800	1,000	975	925	650	620	600
(2) ABS	---	---	---	1,000	925	875	---	---	500
(3) PC I	---	---	---	---	---	---	1,210	1,160	700
(4) Kraton™ G-1651	---	---	100	---	---	100	140	140	100
(5) PPE I	---	---	---	---	---	---	---	80	---
(6) PPE/PMMA blend	---	100	100	---	---	---	---	---	100
(7) PPE/ABS blend	---	---	---	---	100	100	---	---	---
(8) Carbon black	4	---	---	4	---	---	---	---	---
20° Gloss	73	27	24	77	44	35	75	4	29
60° Gloss	88	66	64	93	82	75	99	31	73
85° Gloss	99	93	94	100	97	97	100	87	96

The formulations of the acrylate compositions of Examples 7d to 10d are given below in Table IIId in parts by weight of the total composition. In Table IIId:

- "(1) PMMA" is the same as (1) PMMA in Table IId;
- "(2) PC II" is a polycarbonate having a melt flow rate of 20, available from The  
5 Dow Chemical Company;
- "(3) EXL 4261" is a poly(methyl methacrylate)/phenyl maleimide copolymer, available from Rohm & Haas Company;
- "(4) PET" is Tratuf™ 9506 poly(ethylene terephthalate) having a 0.95 intrinsic viscosity, available from Goodyear Tire and Rubber Company;
- 10 "(5) Kraton™ G 1651" is the same as (7) Kraton™ G 1651 in Table IId;
- "(6) Vectra™ DPX-518" copolymer is a styrene/butadiene/styrene triblock elastomer, available from Dexco;
- "(7) PPE I" is the same as (4) PPE I in Table IId;
- "(8) PPE II" is Noryl™ N-225 poly(phenylene ether)/styrenic polymer alloy having a  
15 deflection temperature under load of 225°F, available from General Electric Company;
- "(9) PPE/PMMA blend" is the same as (5) PPE/PMMA blend in Table IId;
- "(10) PPE/PET blend" is a 50/50 weight ratio blend of poly(phenylene ether) and the poly(ethylene terephthalate) used as component 4, prepared by melt mixing a dry mix of the two polymers at 300°C;
- 20 "(11) Carbon black" is the same as (8) Carbon black in Table IId;
- "(12) Tinuvin™ 327" stabilizer is a phenolic ultra violet light stabilizer, available from Ciba-Geigy Corporation;
- "(13) Chimassorb™ 944 FL" stabilizer is a polymeric hindered amine ultra violet light stabilizer, available from Ciba-Geigy Corporation;
- 25 "(14) IR 1076" is phenolic anti-oxidant stabilizer, available from Ciba-Geigy Corporation;
- "(15) BC-52" is Tetrabromo Bisphenol-A carbonate oligomer, available from Great Lakes Chemical, Inc.;
- "(16) TPP" is triphenyl phosphate, available from Akzo Chemicals, Inc.; and
- 30 "(17) Teflon™ 6C" polymer is a fibril form of poly(tetrafluoroethylene), available from E.I. duPont de Nemours & Co.

In Table IIId, Examples 7d to 10d are indicated by E-7d, E-8d, E-9d and E-10d. Gloss measurements are also performed on the testing samples molded from the compositions of Examples 7d to 10d, and the U.L. 94 burn test is performed on the sample molded from  
35 Example 9d. The results of those measurements are also reported in Table IIId.

Table IIIId

	E-7d	E-8d	E-9d	E-10d
(1) PMMA	900	590	335	---
(2) PC II	-	1,128	1,216	---
(3) EXL 4261	---	---	---	1,800
(4) PET	900	---	---	---
(5) Kraton™ G-1651	100	200	150	---
(6) Vectra™ DPX-518	---	---	---	140
(7) PPE I	---	60	---	---
(8) PPE II	---	---	50	---
(9) PPE/PMMA blend	---	---	---	60
(10) PPE/PET blend	100	---	---	---
(11) Carbon black	---	8	4	---
(12) Tinuvin™ 327	---	5	6	---
(13) Chimassorb™ 944 FL	---	5	---	---
(14) IR 1076	---	4	4	---
(15) BC-52	---	---	100	---
(16) TPP	---	---	120	---
(17) Teflon™ 6C	---	---	15	---
20° Gloss	16	11	10	2
60° Gloss	59	58	52	17
85° Gloss	87	96	88	35
U.L. 94, 1/8"	---	---	5V	---

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The results of the tests performed on the plaques molded from the compositions of Controls Ad to Cd and Examples 1d to 10d demonstrate the lower level of gloss, particularly at 20°, which characterizes the plaques molded from the compositions containing poly(phenylene ether). Small quantities of poly(phenylene ether), 5 weight percent of the composition or less (for  
5 example 4.5 weight percent or less, or 3 weight percent or less), are often sufficient to achieve this effect. The presence of poly(phenylene ether) does not detract from the effect of ignition resistance additives in the blend, as shown by Example 9d. The samples molded from Examples  
1d to 9d showed uniform color with reduced pearlescence and were characterized by reduced delamination effects.

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1. A composition of matter comprising, in admixture,
  - (a) a blend of polycarbonate and polyester; and
  - (b)
    - (i) poly(phenylene ether),
    - (ii) a blend of poly(phenylene ether) with one or more of components (A) to (G), as follows:
      - (A) polystyrene,
      - (B) a random, alternate, block, hydrogenated block or grafted copolymer prepared from a vinyl aromatic compound and one or more members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl methacrylate, ethylene/propylene/diene copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an oxazoline compound,
      - (C) polyamide,
      - (D) polycarbonate,
      - (E) polyester,
      - (F) poly(alkyl acrylate), and
      - (G) poly(alkyl methacrylate); or
    - (iii) a mixture thereof.
2. The composition of Claim 1 wherein the poly(phenylene ether) is present in the composition in an amount of 5 weight percent of the composition or less.
3. The composition of Claim 1 wherein the random, alternate, block, hydrogenated block or grafted copolymer of component (b) is an alkyl acrylate/vinyl aromatic/vinyl nitrile copolymer.
4. The composition of Claim 1 wherein the random, alternate, block, hydrogenated block or grafted copolymer of component (b) is a rubber-modified vinyl nitrile/vinyl aromatic/aryl maleimide copolymer.
5. The composition of Claim 1 wherein component (a) further comprises one or more thermoplastic molding polymers selected from the group consisting of polystyrene, polyolefin, polyamide, poly(vinyl chloride), polyurethane, poly(methyl methacrylate) and polyacetal.
6. The composition of Claim 1 wherein component (a) further comprises one or more elastomeric impact modifiers selected from a thermoplastic elastomer, an olefinic elastomer, or a core-shell elastomer.
7. The composition of Claim 1 further comprising one or more ignition resistance additives selected from halogenated hydrocarbons, halogenated carbonate

oligomers, halogenated diglycidyl ethers, organophosphorous compounds, fluorinated olefins, antimony oxide and metal salts of aromatic sulfur compounds.

8. The composition of Claim 1 in the form of a molded article.

9. The molded article of Claim 8 which has a 20° gloss of less than 65 when  
5 measured according to ASTM Designation D 523-85.

10. A method of molding an article comprising (I) forming a composition by  
melting in a molding machine components (a) and (b) which have not previously been melted  
together, said components (a) and (b) comprising

10 (a) a blend of polycarbonate and polyester; and  
(b) a blend of poly(phenylene ether) with one  
or more of components (i) to (vii), as  
follows:

(i) polystyrene,  
(ii) a random, alternate, block or grafted copolymer prepared  
15 from a vinyl aromatic compound and one or more members  
of the group consisting of a vinyl nitrile compound, a diene,  
an alkyl acrylate, an alkyl methacrylate, glycidyl  
methacrylate, ethylene/propylene/diene copolymer, maleic  
anhydride, an alkyl or aryl maleimide compound, and an  
20 oxazoline compound,  
(iii) polyamide,  
(iv) polycarbonate,  
(v) polyester,  
(vi) poly(alkyl acrylate), and  
25 (viii) poly(alkyl methacrylate); and

(II) molding said article from said composition.

11. The method of Claim 10 wherein component (b) further comprises one or  
more pigments or dyes.

12. A composition of matter comprising, in admixture,  
30 (a) polycarbonate; and  
(b) a blend of poly(phenylene ether) with one or more of  
components (i) to (vii), as follows:

(i) polystyrene,  
(ii) a random, alternate, block, hydrogenated block or  
35 grafted copolymer prepared from a vinyl aromatic  
compound and one or more members of the group  
consisting of a vinyl nitrile compound, a diene, an  
alkyl acrylate, an alkyl methacrylate, glycidyl

methacrylate, ethylene/propylene/diene  
copolymer, maleic anhydride, an alkyl or aryl  
maleimide compound, and an oxazoline  
compound,

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- (iii) polyamide,
- (iv) polycarbonate,
- (v) polyester,
- (vi) poly(alkyl acrylate), and
- (vii) poly(alkyl methacrylate).

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13. The composition of Claim 12 wherein the poly(phenylene ether) is present  
in the composition in an amount of 5 weight percent of the composition or less.

14. The composition of Claim 12 wherein the random, alternate, block,  
hydrogenated block or grafted copolymer of component (b) is a vinyl aromatic/glycidyl  
methacrylate copolymer.

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15. The composition of Claim 12 wherein the random, alternate, block,  
hydrogenated block or grafted copolymer of component (b) is a vinyl  
nitrile/(ethylene/propylene/diene copolymer)/vinyl aromatic copolymer.

16. The composition of Claim 12 wherein component (a) further comprises one  
or more thermoplastic molding polymers selected from the group consisting of polystyrene,  
20 polyolefin, polyamide, poly(vinyl chloride), polygluterimide, polyurethane and polyacetal.

17. The composition of Claim 12 wherein component (a) further comprises one  
or more elastomeric impact modifiers selected from a thermoplastic elastomer, an olefinic  
elastomer, or a core-shell elastomer.

18. The composition of Claim 12 further comprising one or more ignition  
25 resistance additives selected from halogenated hydrocarbons, halogenated carbonate  
oligomers, halogenated diglycidyl ethers, organophosphorous compounds, fluorinated olefins,  
antimony oxide and metal salts of aromatic sulfur compounds.

19. The composition of Claim 12 in the form of a molded article.

20. The molded article of Claim 19 which has a 20° gloss of less than 65 when  
30 measured according to ASTM Designation D 523-85.

21. A method of molding an article comprising (i) forming a composition by  
melting in a molding machine components (a) and (b) which have not previously been melted  
together, said components (a) and (b) comprising

- (a) polycarbonate; and
- 35 (b) a blend of poly(phenylene ether) with one  
or more of components (i) to (vii), as  
follows:

(i) polystyrene,



- 5 (ii) a random, alternate, block or grafted copolymer prepared from a vinyl aromatic compound and one or more members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl methacrylate, ethylene/propylene/diene copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an oxazoline compound,
- 10 (iii) polyamide,  
(iv) polycarbonate,  
(v) polyester,  
(vi) poly(alkyl acrylate), and  
(viii) poly(alkyl methacrylate); and
- (II) molding said article from said composition.

22. The method of Claim 21 wherein component (b) further comprises one or  
15 more pigments or dyes.

23. A composition of matter comprising, in admixture,
- (a) a random, alternate, block or grafted copolymer prepared from a vinyl aromatic compound and one or more members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl methacrylate, ethylene/propylene/diene copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an oxazoline compound; and
- 20 (b) (i) poly(phenylene ether),  
(ii) a blend of poly(phenylene ether) with one or more of components (A) to (G), as follows:  
(A) polystyrene,  
(B) a random, alternate, block, hydrogenated block or grafted copolymer prepared from a vinyl aromatic compound and one or more members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl methacrylate, ethylene/propylene/diene copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an oxazoline compound,  
(C) polyamide,  
(D) polycarbonate,
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- (E) polyester,
- (F) poly(alkyl acrylate), and
- (G) poly(alkyl methacrylate); or

(iii) a mixture thereof.

- 5           24. The composition of Claim 23 wherein the poly(phenylene ether) is present in the composition in an amount of 5 weight percent of the composition or less.
25. The composition of Claim 23 wherein the random, alternate, block, hydrogenated block or grafted copolymer of component (a) or (b) is a vinyl aromatic/maleic anhydride copolymer.
- 10          26. The composition of Claim 23 wherein the random, alternate, block, hydrogenated block or grafted copolymer of component (a) or (b) is a vinyl aromatic/oxazoline copolymer.
27. The composition of Claim 23 wherein the random, alternate, block, hydrogenated block or grafted copolymer of component (a) or (b) is a rubber-modified vinyl
- 15 aromatic/vinyl nitrile/alkyl methacrylate copolymer.
28. The composition of Claim 23 wherein component (a) further comprises one or more thermoplastic molding polymers selected from the group consisting of polyester, polystyrene, polyolefin, polyamide, poly(vinyl chloride), polyurethane and polyacetal.
29. The composition of Claim 23 wherein component (a) further comprises one
- 20 or more elastomeric impact modifiers selected from a thermoplastic elastomer, an olefinic elastomer, or a core-shell elastomer.
30. The composition of Claim 24 further comprising one or more ignition resistance additives selected from halogenated hydrocarbons, halogenated carbonate oligomers, halogenated diglycidyl ethers, organophosphorous compounds, fluorinated olefins,
- 25 antimony oxide and metal salts of aromatic sulfur compounds.
31. The composition of Claim 23 in the form of a molded article.
32. A method of molding an article comprising (i) forming a composition by melting in a molding machine components (a) and (b) which have not previously been melted together, said components (a) and (b) comprising
- 30           (a) a random, alternate, block or grafted copolymer prepared from a vinyl aromatic compound and one or more members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl methacrylate, ethylene/propylene/diene copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an oxazoline
- 35           compound; and
- (b) a blend of poly(phenylene ether) with one or more of components (i) to (vii), as follows:

- 5 (i) polystyrene,  
 (ii) a random, alternate, block or grafted copolymer prepared from a vinyl aromatic compound and one or more members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl methacrylate, ethylene/propylene/diene copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an oxazoline compound,
- 10 (iii) polyamide,  
 (iv) polycarbonate,  
 (v) polyester,  
 (vi) poly(alkyl acrylate), and  
 (vii) poly(alkyl methacrylate); and
- (II) molding said article from said composition.
- 15 33. The method of Claim 32 wherein component (b) further comprises one or more pigments or dyes.
34. A composition of matter comprising, in admixture,
- (a) (i) poly(alkyl acrylate),  
 (ii) poly(alkyl methacrylate),  
 20 (iii) a copolymer prepared from (A) an alkyl acrylate, an alkyl methacrylate, or a mixture thereof, and (B) one or more ethylenically unsaturated monomers, or  
 (iv) a mixture thereof; and
- (b) (i) poly(phenylene ether),  
 25 (ii) a blend of poly(phenylene ether) with one or more of components (A) to (G), as follows:  
 (A) polystyrene,  
 (B) a random, alternate, block, hydrogenated block or grafted copolymer prepared from a vinyl aromatic compound and one or more members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl methacrylate, ethylene/propylene/diene copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an oxazoline compound,  
 30 (C) polyamide,  
 (D) polycarbonate,
- 35

(E) polyester,

(F) poly(alkyl acrylate), and

(G) poly(alkyl methacrylate); or

(iii) a mixture thereof.

5           35. The composition of Claim 34 wherein the poly(phenylene ether) is present in the composition in an amount of 5 weight percent of the composition or less.

36. The composition of Claim 34 wherein said ethylenically unsaturated monomer is described by

$R_1-C \equiv C-R_2$ , where each R is independently

10           (A) (1) hydrogen; (2) a halogen; (3) -OH; (4) -CO<sub>2</sub>H; (5) -SH; (6) -CN; (7) -NO<sub>2</sub>; or (8) -C<sub>1</sub>-C<sub>8</sub>Z; (9) -C(O)Z; (10) -CO<sub>2</sub>Z; (11) -CO<sub>2</sub>NZ<sub>2</sub>; (12) -OZ; (13) -SZ; (14) -SOZ; (15) -SO<sub>2</sub>Z; (16) -NZ<sub>2</sub>; or (17) -PZ<sub>3</sub> (where Z is H, halogen, O, -OH, -CO<sub>2</sub>H, -SH, -CN, -NO<sub>2</sub> or an epoxide ring; or a C<sub>1</sub>-C<sub>10</sub> linear or branched, saturated or unsaturated, alkyl radical or a C<sub>6</sub>-C<sub>14</sub> aryl radical substituted with halogen, -OH, -CO<sub>2</sub>H, -SH, -CN, -NO<sub>2</sub> or an epoxide ring); or  
15           (B) a C<sub>1</sub>-C<sub>10</sub> linear or branched, saturated or unsaturated, alkyl radical optionally substituted with, or interruptible with, a phenyl radical or one or more members of group (A); or  
20           (C) a phenyl or naphthyl radical, each independently optionally substituted with a C<sub>1</sub>-C<sub>6</sub> linear or branched alkyl radical or one or more members of group (A).

37. The composition of Claim 34 wherein component (a) is a copolymer of  
25 methyl methacrylate and phenyl maleimide.

38. The composition of Claim 34 wherein the vinyl aromatic copolymer of component (b) is a vinyl aromatic/oxazoline copolymer.

39. The composition of Claim 34 wherein the vinyl aromatic copolymer of component (b) is a rubber-modified vinyl nitrile/vinyl aromatic/aryl maleimide copolymer.

30           40. The composition of Claim 34 wherein component (a) further comprises one or more thermoplastic molding polymers selected from the group consisting of polycarbonate, polyester, polystyrene, polyolefin, polyamide, poly(vinyl chloride), polyurethane and polyacetal.

41. The composition of Claim 34 further comprising one or more elastomeric  
35 impact modifiers selected from a thermoplastic elastomer, an olefinic elastomer, or a core-shell elastomer.

42. The composition of Claim 34 further comprising one or more ignition resistance additives selected from halogenated hydrocarbons, halogenated carbonate

oligomers, halogenated diglycidyl ethers, organophosphorous compounds, fluorinated olefins, antimony oxide and metal salts of aromatic sulfur compounds.

43. The composition of Claim 34 in the form of a molded article.

44. The molded article of Claim 43 which has a 20° gloss of less than 70 when  
5 measured according to ASTM Designation D 523-85.

45. A method of molding an article comprising (I) forming a composition by melting in a molding machine components (a) and (b) which have not previously been melted together, said components (a) and (b) comprising

(a) (i) poly(alkyl acrylate),

10 (ii) poly(alkyl methacrylate),

(iii) a copolymer prepared from (A) an alkyl acrylate, an alkyl methacrylate, or a mixture thereof, and (B) one or more ethylenically unsaturated monomers, or

(iv) a mixture thereof; and

15 (b) a blend of poly(phenylene ether) with one

or more of components (i) to (vii), as

follows:

(i) polystyrene,

20 (ii) a random, alternate, block or grafted copolymer prepared from a vinyl aromatic compound and one or more members of the group consisting of a vinyl nitrile compound, a diene, an alkyl acrylate, an alkyl methacrylate, glycidyl methacrylate, ethylene/propylene/diene copolymer, maleic anhydride, an alkyl or aryl maleimide compound, and an  
25 oxazoline compound,

(iii) polyamide,

(iv) polycarbonate,

(v) polyester,

(vi) poly(alkyl acrylate), and

30 (viii) poly(alkyl methacrylate); and

(II) molding said article from said composition.

46. The method of Claim 45 wherein component (b) further comprises one or more pigments or dyes.

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## INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

<b>(51) International Patent Classification <sup>5</sup> :</b> C08L 69/00, 67/02, 53/00 C08L 51/00, 71/12, 101/00	<b>A3</b>	<b>(11) International Publication Number:</b> WO 93/19128 <b>(43) International Publication Date:</b> 30 September 1993 (30.09.93)												
<b>(21) International Application Number:</b> PCT/US93/02176 <b>(22) International Filing Date:</b> 10 March 1993 (10.03.93)  <b>(30) Priority data:</b> <table border="0"><tr><td>07/850,324</td><td>10 March 1992 (10.03.92)</td><td>US</td></tr><tr><td>07/850,329</td><td>10 March 1992 (10.03.92)</td><td>US</td></tr><tr><td>07/850,335</td><td>10 March 1992 (10.03.92)</td><td>US</td></tr><tr><td>07/851,371</td><td>10 March 1992 (10.03.92)</td><td>US</td></tr></table> <b>(71) Applicant:</b> THE DOW CHEMICAL COMPANY [US/US]; 2030 Dow Center, Abbott Road, Midland, MI 48640 (US). <b>(72) Inventor:</b> LAUGHNER, Michael, K. ; 1403 North Road, Lake Jackson, TX 77566 (US). <b>(74) Agent:</b> LANGWORTHY, John, A.; The Dow Chemical Company, Patent Dept., B-1211, Freeport, TX 77541 (US).		07/850,324	10 March 1992 (10.03.92)	US	07/850,329	10 March 1992 (10.03.92)	US	07/850,335	10 March 1992 (10.03.92)	US	07/851,371	10 March 1992 (10.03.92)	US	<b>(81) Designated States:</b> CA, JP, European patent (AT, BE, CH, DE, DK, ES, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE).  <b>Published</b> <i>With international search report. Before the expiration of the time limit for amending the claims and to be republished in the event of the receipt of amendments.</i>  <b>(88) Date of publication of the international search report:</b> 25 November 1993 (25.11.93)
07/850,324	10 March 1992 (10.03.92)	US												
07/850,329	10 March 1992 (10.03.92)	US												
07/850,335	10 March 1992 (10.03.92)	US												
07/851,371	10 March 1992 (10.03.92)	US												
<b>(54) Title:</b> POLYMERS AND POLYMER BLENDS MODIFIED WITH POLY(PHENYLENE ETHER)  <b>(57) Abstract</b> <p>A matrix resin such as a polycarbonate/polyester blend, a polycarbonate, a vinyl aromatic copolymer or an acrylate polymer or copolymer is admixed in a composition with poly(phenylene ether), and/or with a poly(phenylene ether) concentrate containing poly(phenylene ether), polystyrene, a vinyl aromatic copolymer, polyamide, polycarbonate, polyester, poly(alkyl acrylate), and/or poly(alkyl methacrylate). The compositions may also optionally contain additional vinyl aromatic copolymer as a separate component, impact modifiers, thermoplastic molding materials including polystyrene, polyolefin, polyamide, poly(vinyl chloride), polyurethane, poly(methyl methacrylate) and polyacetal, and conventional additives such as dyes and pigments. The compositions when molded, particularly when the poly(phenylene ether) content thereof is low (for example, 5 weight percent or less) show a desirably low gloss, and a desirable balance of other properties.</p>														

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# INTERNATIONAL SEARCH REPORT

International Application No.

PCT/US 93/02176

<b>I. CLASSIFICATION OF SUBJECT MATTER</b> (If several classification symbols apply, indicate all) <sup>6</sup>		
According to International Patent Classification (IPC) or to both National Classification and IPC		
Int. Cl. 5	C 08 L 69/00	C 08 L 67/02
C 08 L 51/00	C 08 L 71/12	C 08 L 101/00
<b>II. FIELDS SEARCHED</b>		
Minimum Documentation Searched <sup>7</sup>		
Classification System	Classification Symbols	
Int. Cl. 5	C 08 L	
Documentation Searched other than Minimum Documentation to the Extent that such Documents are Included in the Fields Searched <sup>8</sup>		
<b>III. DOCUMENTS CONSIDERED TO BE RELEVANT<sup>9</sup></b>		
Category *	Citation of Document, <sup>11</sup> with indication, where appropriate, of the relevant passages <sup>12</sup>	Relevant to Claim No. <sup>13</sup>
X	EP, A, 0382548 (SUMITOMO CHEMICAL COMPANY) 16 August 1990 see the whole document ---	1-11
X	EP, A, 0306774 (GENERAL ELECTRIC COMPANY) 15 March 1989 see page 10, line 49 - page 11, line 9; claims 1-26 ---	1,3-11
X	WO, A, 8700850 (GENERAL ELECTRIC COMPANY) 12 February 1987 see claims 1-33 ---	1,3-11
X	EP, A, 0208940 (GENERAL ELECTRIC COMPANY) 21 January 1987 see the whole document ---	1-11
	-/-	
<div style="display: flex; justify-content: space-between;"> <div style="width: 45%;"> <p>* Special categories of cited documents: <sup>10</sup></p> <p>"A" document defining the general state of the art which is not considered to be of particular relevance</p> <p>"E" earlier document but published on or after the international filing date</p> <p>"L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)</p> <p>"O" document referring to an oral disclosure, use, exhibition or other means</p> <p>"P" document published prior to the international filing date but later than the priority date claimed</p> </div> <div style="width: 45%;"> <p>"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention</p> <p>"X" document of particular relevance; the claimed invention cannot be considered novel or cannot be considered to involve an inventive step</p> <p>"Y" document of particular relevance; the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art.</p> <p>"A" document member of the same patent family</p> </div> </div>		
<b>IV. CERTIFICATION</b>		
Date of the Actual Completion of the International Search	Date of Mailing of this International Search Report	
30-06-1993	22 JUN 93	
International Searching Authority	Signature of Authorized Officer	
EUROPEAN PATENT OFFICE	DECOCKER	

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III. DOCUMENTS CONSIDERED TO BE RELEVANT (CONTINUED FROM THE SECOND SHEET)		
Category *	Citation of Document, with indication, where appropriate, of the relevant passages	Relevant to Claim No.
P,X	WO,A,9215643 (THE DOW CHEMICAL COMPANY) 17 September 1992 see claims 1-14 ----	1-11
A	EP,A,0336195 (GENERAL ELECTRIC COMPANY) 11 October 1989 see claims 1-8; table 1 ----	1
A	EP,A,0229957 (GENERAL ELECTRIC COMPANY) 29 July 1987 see claims 1-18 -----	1

Form PCT/ISA/210 (extra sheet) (January 1983)

# INTERNATIONAL SEARCH REPORT

International application No.

PCT/US 93/02176

## Box I Observations where certain claims were found unsearchable (Continuation of item 1 of first sheet)

This international search report has not been established in respect of certain claims under Article 17(2)(a) for the following reasons:

1. ☐ Claims Nos.:  
because they relate to subject matter not required to be searched by this Authority, namely:
2. ☐ Claims Nos.:  
because they relate to parts of the international application that do not comply with the prescribed requirements to such an extent that no meaningful international search can be carried out, specifically:
3. ☐ Claims Nos.:  
because they are dependent claims and are not drafted in accordance with the second and third sentences of Rule 6.4(a).

## Box II Observations where unity of invention is lacking (Continuation of item 2 of first sheet)

This International Searching Authority found multiple inventions in this international application, as follows:

1: Claims 1-11  
2: Claims 12-22  
3: Claims 23-33  
4: Claims 34-46

1. ☐ As all required additional search fees were timely paid by the applicant, this international search report covers all searchable claims.
2. ☐ As all searchable claims could be searched without effort justifying an additional fee, this Authority did not invite payment of any additional fee.
3. ☒ As only some of the required additional search fees were timely paid by the applicant, this international search report covers only those claims for which fees were paid, specifically claims Nos.:  
1-11
4. ☐ No required additional search fees were timely paid by the applicant. Consequently, this international search report is restricted to the invention first mentioned in the claims; it is covered by claims Nos.:

Remark on Protest

- ☐ The additional search fees were accompanied by the applicant's protest.  
☐ No protest accompanied the payment of additional search fees.

**ANNEX TO THE INTERNATIONAL SEARCH REPORT  
ON INTERNATIONAL PATENT APPLICATION NO.**

US 9302176  
SA 71664

This annex lists the patent family members relating to the patent documents cited in the above-mentioned international search report. The members are as contained in the European Patent Office EDP file on 13/10/93. The European Patent Office is in no way liable for these particulars which are merely given for the purpose of information.

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		EP-A- 0352822	31-01-90
		JP-A- 62169850	27-07-87

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